

DISPENSA

DISPENSA DI

MECCANICA DEI

FLUIDI

DI

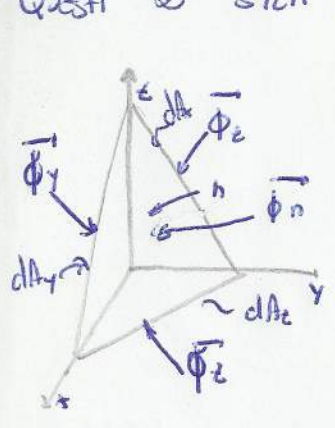
PIETRO

ACETI

MECCANICA DEI FLUIDI

- STATI DI SFORTO

In un punto di fluido \exists 3 velocità e ∞ stati di sforzo dipendenti dalle sup. considerate. Questi ∞ stati di sforzo possono essere ricondotti a solo 3 grazie al tetraedro di Cauchy.



INFINITESIMI 2° ORDINE INFINITESIMI 3° ORDINE

$$\sum \vec{F}_{sup} + \sum \vec{F}_{ms} = 0$$

$$\vec{\Phi}_n dA_n = \vec{\Phi}_x dA_x + \vec{\Phi}_y dA_y + \vec{\Phi}_z dA_z$$

$$\vec{\Phi}_n dA = \vec{\Phi}_x dA \cos \hat{n}_x + \vec{\Phi}_y dA \cos \hat{n}_y + \vec{\Phi}_z dA \cos \hat{n}_z$$

$$\vec{\Phi}_n = \vec{\Phi}_x \cos \hat{n}_x + \vec{\Phi}_y \cos \hat{n}_y + \vec{\Phi}_z \cos \hat{n}_z \quad \text{ETTORE}$$

$$\Phi_{nx} = \Phi_{xx} \cos \hat{n}_x + \Phi_{yx} \cos \hat{n}_y + \Phi_{zx} \cos \hat{n}_z$$

$$\Phi_{xy}$$

$$\vec{\Phi} = \begin{bmatrix} \sigma_x & \tau_{xy} & \tau_{xz} \\ \tau_{yx} & \sigma_y & \tau_{yz} \\ \tau_{zx} & \tau_{zy} & \sigma_z \end{bmatrix}$$

ESEMPIO: sempre lungo x

• IDROSTATICA

Un fluido in quiete non ha spostamenti relativi tra le particelle $\Rightarrow \tau_x = \tau_y = \tau_z = 0$
 \exists solo sforzi normali indipendenti dall'orientazione $\rightarrow \sigma_x = \sigma_y = \sigma_z = p$

• PROPRIETÀ FISICHE

- ① DENSITÀ: massa contenuta nell'unità di volume $\frac{kg}{m^3} = \rho$
- ② PESO SPECIFICO: il peso dell'unità di volume $\frac{N}{m^3} = \frac{kg \cdot a}{m^3} = \rho g = \gamma$
- ③ COMPRESSIBILITÀ

Se applico una differenza di pressione Δp a una dif. di volume prop. di V iniziale e a cost. del fluido

$$dW = - \frac{W}{E} dp \quad (1)$$

Poiché la massa $m = \text{cost}$ $\rho W = \text{cost} \rightarrow d(\rho W) = 0 \Rightarrow \rho dW + W dp = 0 \Rightarrow -\frac{dW}{W} = \frac{dp}{\rho}$

dalla ① $\rightarrow -\frac{dW}{W} = \frac{dp}{\rho} \Rightarrow \frac{dp}{\rho} = \frac{dp}{E} \Rightarrow \text{INTEGRA INTRA } \begin{matrix} p \in p_0 \\ \rho \in \rho_0 \end{matrix} \Rightarrow \ln\left(\frac{\rho}{\rho_0}\right) = \frac{p-p_0}{E}$

$$\rho = \rho_0 e^{\frac{(p-p_0)}{E}}$$

$$\rho = \rho_0 \left[1 + \frac{p-p_0}{E} \right]$$

④ VISCOSITÀ



$$T = \mu A \frac{\Delta v}{\Delta r}$$

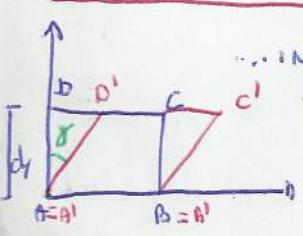
$$\tau = \mu \frac{\Delta v}{\Delta r}$$

La forza resist. T è proporzionale all'area A e all'incremento di velocità che agito fra Δr alla distanza r .
 ⑤ μ è un coef. che dipende dal fluido.

$$\tau = \mu \frac{\partial v}{\partial r} \quad \text{LEGGE DI NEWTON}$$

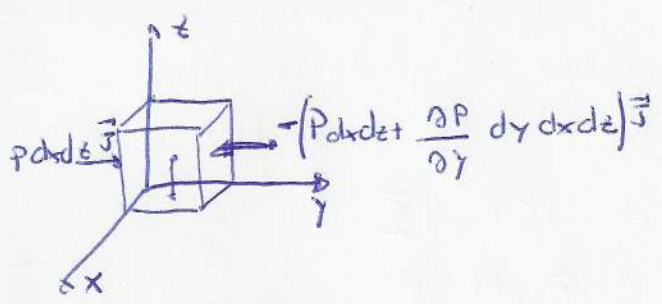
N.B. QUANDO VARIA v ho le τ
 se $\Delta v = 0 \Rightarrow \tau = 0$ non ho sforzi τ in un fluido in quiete

⑤ FLUIDI NEWTONIANI



$v_A = v_B = v = v_C = v + \frac{dv}{dy} dy$
 ... IN UN ISTANTE dt ...
 $dx = \tau dy = \frac{dv}{dy} dy dt \Rightarrow \frac{dx}{dt} = \frac{dv}{dy}$
 DALLA L. DI NEWTON $= \frac{dx}{dt} = \frac{\tau}{\mu} \Rightarrow \tau = \mu \frac{dx}{dt}$
 LA VELOCITÀ DI DEF. ANGOLARE È PROP. AL τ E DIPENDE DA μ

EQ INDEFINITA STATICA DEI FLUIDI



$$\sum \vec{F}_m + \sum \vec{F}_s = 0$$

$$\int_V \vec{F} dxdydz = \left(\frac{\partial p}{\partial x} \vec{i} + \frac{\partial p}{\partial y} \vec{j} + \rho \frac{\partial p}{\partial z} \vec{k} \right) dxdydz$$

$$\rho \vec{F} = \text{grad}(p)$$

EQ INDEF. DELLA STATICA DEI FLUIDI

$L_{x/y} = \Delta z = \gamma$

FLUIDO PESANTE ($\vec{F} = \vec{j}$) INCOMPRESSIBILE ($\rho = \text{cost}$)

$$-\gamma \text{grad}(z)$$

VALE PER $\rho = \rho^*$

LEGE DI STEVIN

$$\Rightarrow \rho g \text{grad}(z) + \text{grad}(p) = 0 \Rightarrow \gamma \nabla z + \nabla p = 0 \Rightarrow \nabla z + \nabla \left(\frac{p}{\gamma} \right) = 0 \Rightarrow \nabla \left(z + \frac{p}{\gamma} \right) = 0$$

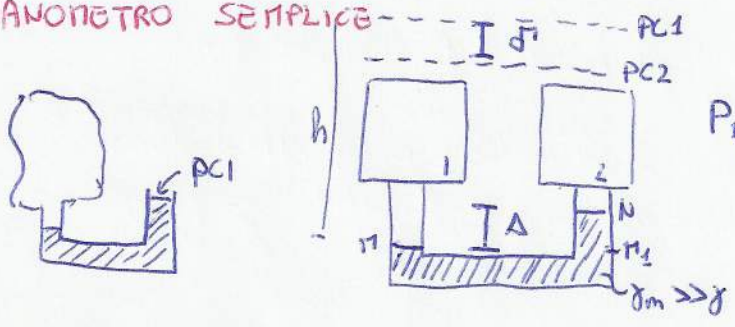
$$z + \frac{p}{\gamma} = \text{cost}$$

h geometrica
 h di pressione
 h piezometrica

NB: Lungo le sup equipotenziali la pressione è la stessa. $p = (\text{cost} - \gamma) \gamma$

$F = \Delta U$ (Forze conservative) $\rightarrow \rho \Delta U = \Delta p \rightarrow$ su una sup equi $\Delta U = \text{cost} \rightarrow \Delta p = 0 \rightarrow p = \text{cost}$

MANOMETRO SEMPLICE



$$P_{N_1} = P_N + \Delta \gamma m = \gamma (h - \Delta - \delta) + \Delta \gamma m = \gamma h$$

$$-\Delta \gamma - \delta' \gamma + \Delta \gamma m = 0$$

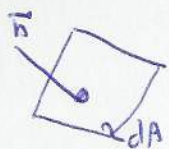
$$\delta' = \frac{\Delta (\gamma m - \gamma)}{\gamma}$$

se $\gamma_m \leq \gamma \Rightarrow \delta' = \frac{\Delta (\gamma - \gamma_m)}{\gamma}$

se $\gamma_1 \neq \gamma_2$

$$\delta' = \frac{h (\gamma_2 - \gamma_1) + \Delta (\gamma_m - \gamma_2)}{\gamma_2}$$

SPINTE IDROSTATICHE



Def: $d\vec{s} = p dA \vec{n}$

$\vec{S} = \int_A p \vec{n} dA$

DI UNA SPINTA BISOGNA CONOSCERE: ① TITO D'ORO ② DIR ③ VERSO ④ P.TO DI APPLICAZIONE

• SPINTE SUP. PIANE

sup piano $\vec{n} = \text{cost}$

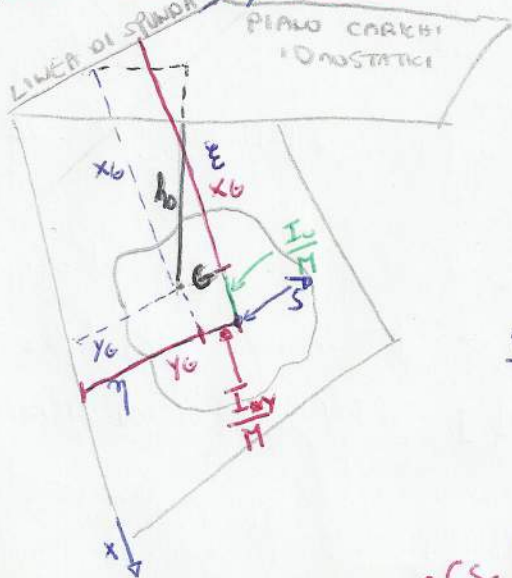
$|S| = \int_A p dA = pA$

- DIR \perp al fluido e usante da esso
- BARICENTRO \bar{c} il p.to di applicazione se la pressione \bar{c} costante



A = modulo

• SPINTA SU SUP. INCLINATA



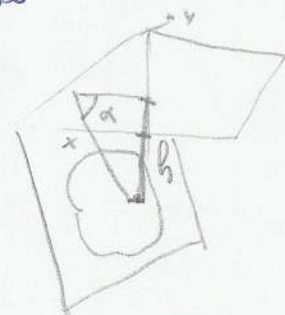
$|S| = \int_A p dA = \int_A \gamma x \sin \alpha dA = \gamma \sin \alpha \int_A x dA = \gamma \sin \alpha x_G A$

$|S| = \gamma h_G A = P_G A$

$S_x = \int_A p dA x = \int_A \gamma h dA x =$

$\int_A \gamma x \sin \alpha x dA = \gamma \sin \alpha \int_A x^2 dA$

$\eta = \frac{\gamma \sin \alpha \int_A x^2 dA}{\gamma \sin \alpha \int_A x dA} = \frac{\int_A x^2 dA}{\int_A x dA} = \frac{I}{M}$



AFFONDAMENTO BARICENTRO

• SPINTA LA CALCA SULL'ANCA

• il centro invece le angole inclinate

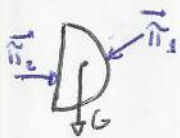
$C.S. = \left(x_G + \frac{I_0}{M x_G}, d \right)$

$x_G = \text{AFFONDAMENTO DI } P_G \text{ SIMBOLICO}$
 $I_0 = \text{DELLA FIGURA VISTA } \perp$
 $M = x_G A$

$\eta = \frac{I_{xy}}{M} = \frac{\int xy dA}{\int x dA} = x_G A$

• SUP. CURVE

① EQUILIBRIO GLOBALE: RIVOLUCO SUP. CURVE ALLA SOMMA DI SUP. PIANE



$\vec{\pi}_1 + \vec{\pi}_2 + \vec{G} = 0$
 $\vec{S} = -\vec{\pi}_1$

$-\vec{\pi}_1 = \vec{G} + \vec{\pi}_2$

② METODO DELLE COMPONENTI: SCOMPONGO LA SPINTA CURVA IN 3 SPINTE PIANE

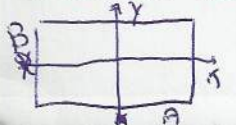
$dS_x = p dA_x \rightarrow S_x = \int p dA_x = \gamma h_{Gx} A_x$
 $dS_y = p dA_y \rightarrow S_y = \int p dA_y = \gamma h_{Gy} A_y$
 $dS_z = p dA_z \rightarrow S_z = \int p dA_z = \text{peso} = \gamma W$

$x_1 = x_0 + x'$

$\eta = \frac{I}{M} = \frac{\int x^2 dA}{\int x dA} = \frac{x_0^2 A + \int x'^2 dA}{x_0 A + \int x' dA} = x_0 + \frac{I_0}{x_0}$

momento di inerzia rispetto a un asse baricentrico // alle linee di spinta

momenti di I_{xy}



$I_{xx} = \frac{A B^3}{12}$ $I_{yy} = \frac{B A^3}{12}$

CINEMATICA

LAGRANGE: SI SEQUE UNA PARTICELLA V VARIA nello spazio e nel tempo $\frac{d}{dt}$

EULERO: SI FISSA UN VOLUME E SI GUARDA COSA PASSA: V viene solo nel tempo $\frac{\partial}{\partial t}$

$$\vec{V} = \vec{V}(x, y, z, t)$$

$$\vec{V} = u \vec{i} + v \vec{j} + w \vec{k} \quad \text{con} \quad u = \frac{dx}{dt} \quad v = \frac{dy}{dt} \quad z = \frac{dz}{dt}$$

$$a = \frac{d\vec{V}}{dt} = \frac{d\vec{V}(x(t); y(t); z(t); t)}{dt} = \frac{\partial \vec{V}}{\partial t} + \left(\frac{\partial \vec{V}}{\partial x} u + \frac{\partial \vec{V}}{\partial y} v + \frac{\partial \vec{V}}{\partial z} w \right)$$

ACC. CONV.: come V varia con la posizione. non è lineare \rightarrow origine turbolenze

ACC. LOCALE: come varia \vec{V} solo rispetto al tempo $\neq 0$ solo per moti non stazionari

LINEA DI CORRENTE: È UNA LINEA γ in ogni punto la vettore velocità del punto

TUBO DI FLUSSO: tra le linee di corrente posso delimitare una regione chiusa tubo di flusso dove non ho correnti \perp ad esso.

INB. una condotta è un tubo di flusso.

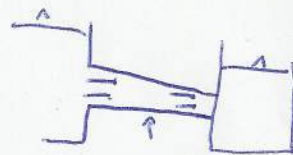
TIPICI DI MOTI:

Permanente: \vec{V} varia nello spazio ma non nel tempo

$$\vec{V} = \vec{V}(x, y, z)$$

Uniforme: Non varia
 $\vec{V} = \omega s t$

STAZIONARI



Stazionario

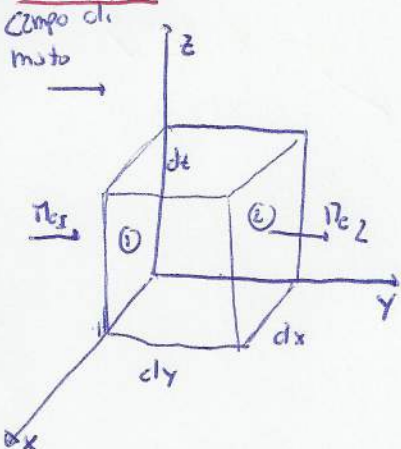
VARIO: il moto varia.

$$d[\rho(gx)] = \frac{d\rho}{dg} \frac{dg}{dx} = D(3x)^2 = \frac{d(3x)^2}{d(3x)} \cdot \frac{d3x}{dx} \quad 2 \cdot 3x \cdot 3 =$$

$$a = \frac{d\vec{V}}{dt} = \frac{\partial \vec{V}}{\partial t} + \frac{\partial \vec{V}}{\partial x} \frac{dx}{dt}$$

EQUAZIONI DI CONTINUITÀ: conservazione della massa

INDEFINITA



Nel volume considerato zero $M = \rho \, dx \, dy \, dz$

In ① $\Pi_I = \rho \, v \, dx \, dz \, dt$

$$\frac{kg}{m^3} \frac{m}{s} m \, m \, m \, s = kg$$

In ② $\Pi_{II} = \Pi_I + \frac{\partial \Pi_I}{\partial y} \, dy$

ENTRANTE - USCENTE = $\Pi_I - \Pi_{II} - \frac{\partial \Pi_I}{\partial y} \, dy = - \frac{\partial (\rho v)}{\partial y} \, dx \, dz \, dt \, dy$

$$\Delta M = - \frac{\partial}{\partial x} (\rho u) \, dx \, dy \, dz \, dt - \frac{\partial}{\partial y} (\rho v) \, dx \, dy \, dz \, dt - \frac{\partial}{\partial z} (\rho w) \, dx \, dy \, dz \, dt$$

$$\Delta M = \frac{\partial \rho}{\partial t} \, dx \, dy \, dz \, dt = \frac{dm}{dt} = \frac{\partial (\rho \, dx \, dy \, dz)}{\partial t} \, dt = \frac{\partial \rho}{\partial t} \, dx \, dy \, dz \, dt$$

VAR. MASSA NEL VOLUME

L. $\frac{\partial \rho}{\partial t} + \text{div}(\rho \vec{v}) = 0$

FLUSSO sulla sup. di contorno

Riscrivendo: $\frac{\partial \rho}{\partial t} + \rho \frac{\partial v_x}{\partial x} + \rho \frac{\partial v_y}{\partial y} + \rho \frac{\partial v_z}{\partial z} + v_x \frac{\partial \rho}{\partial x} + v_y \frac{\partial \rho}{\partial y} + v_z \frac{\partial \rho}{\partial z} + \rho \frac{\partial v_x}{\partial x} + \rho \frac{\partial v_y}{\partial y} + \rho \frac{\partial v_z}{\partial z}$

Complete $\frac{\partial \rho}{\partial t} + \rho \text{div}(\vec{v}) = 0$

$\rho = \text{cost}$
FLUIDO INCOMPRESSIBILE

$\text{div}(\vec{v}) = 0$

NON ASSO DINE CHE È STAZIONARIO. HA ASSO DINE CHE È COST IGLO CHE DIVERGENTE SE IL MULO È MONODIREZIONALE

GLOBALI → integrale

$$\frac{\partial \rho}{\partial t} + \text{div}(\rho \vec{v}) = 0 \Rightarrow \int_W \frac{\partial \rho}{\partial t} \, dW + \int_W \text{div}(\rho \vec{v}) \, dW = 0$$

come varia la m nel kw entrate meno uscite

$$\frac{\partial}{\partial t} \int_W \rho \, dW = \int_A \rho \vec{v} \cdot \vec{n} \, dA \Rightarrow \frac{\partial}{\partial t} \int_W \rho \, dW = \int_A \rho v_n \, dA$$

$\frac{\partial}{\partial t} \int_W \rho \, dW = \int_A \rho v_n \, dA$

THE STOKES $\int_W \text{div}(F) \, dW = \int_A \vec{F} \cdot \vec{n} \, dA$

$\Rightarrow \rho = \text{cost}$

$\frac{\partial m}{\partial t} = \rho \int_A v_n \, dA \Rightarrow \int_A v_n \, dA = 0 \Rightarrow Q_E = Q_U$

$\int_A v_n \, dA = \text{PORTATA VOLUMETRICA}$

$\frac{m}{s} \, m^3 = \frac{m^3}{s} = \dot{V}$

TUBI DI FLUSSO



$\Pi_{inlet} = \rho A v \, ds$
 $\Pi_{out} = \rho Q \, dt$
 $\Pi_{us} = \rho Q \, dt + \frac{\partial (\rho Q)}{\partial s} \, ds \, dt$

VARIAZIONE entrate ed uscite $\Rightarrow - \frac{\partial (\rho Q)}{\partial s} \, ds \, dt = \frac{\partial (\rho A)}{\partial t} \, ds \, dt$

$\frac{\partial (\rho A)}{\partial t} + \frac{\partial (\rho Q)}{\partial s} = 0$

LA PORTATA LINGO S VARIA DALLA SEZIONE

FLUIDO INCOMPRESSIBILE $\rho = \text{cost}$

$\rho \frac{dA}{dt} + \rho \frac{dQ}{ds} = 0 \rightarrow$ LA PORTATA È COSTANTE QUINDI $\frac{\partial A}{\partial t} = 0$

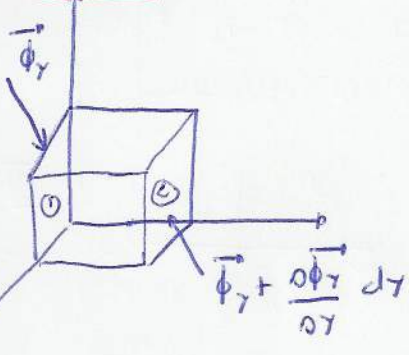
NON PERTINENTE CANTATA INDEFINIBILI

- PER UN NUDO PERMANENTE oppure - PER UNA CANTATA INDEF.

$Q_{iniziale} = Q_{finale}$

BILANCIO QUANTITÀ DI MOTO : EQUILIBRIO DINAMICO

INDEFINITA



$$\sum \vec{F} = m \vec{a}$$

$$\sum \vec{F}_s + \sum \vec{F}_m = m \vec{a}$$

$$\sum \vec{F}_m = \rho \vec{f} dx dy dz$$

$$\sum \vec{F}_s = \int_{\text{LUNGO } Y} (\vec{\phi}_y - \vec{\phi}_y - \frac{\partial \vec{\phi}_y}{\partial y} dy) dx dz \quad \text{ANALOGO PER } x, z$$

$$\rho \vec{f} dx dy dz - \frac{\partial \vec{\phi}_x}{\partial x} dx dy dz - \frac{\partial \vec{\phi}_y}{\partial y} dx dy dz - \frac{\partial \vec{\phi}_z}{\partial z} dx dy dz = \rho dx dy dz \vec{a}$$

$\rho (\vec{f} - \vec{z})$: distruzione degli sforzi
 - forze (forzante) - termini cinematici

$$\underline{\underline{\phi}} = \begin{bmatrix} \sigma_x & \tau_{xz} & \tau_{xy} \\ \tau_{xz} & \sigma_y & \tau_{yx} \\ \tau_{xy} & \tau_{yx} & \sigma_z \end{bmatrix}$$

GALE

$$\int_W \rho \vec{f} dW - \int_W \rho \vec{z} dW = \int_W \frac{\phi_x}{\partial x} dW + \int_W \frac{\phi_y}{\partial y} dW + \int_W \frac{\phi_z}{\partial z} dW$$

① $\vec{G} = m \vec{f}$

② $\rho \vec{z} = \rho \frac{d\vec{v}}{dt} = \rho \frac{d\vec{v}}{dt} + \rho u \frac{d\vec{v}}{dx} + \rho v \frac{d\vec{v}}{dy} + \rho w \frac{d\vec{v}}{dz}$

$$= \rho \frac{d\vec{v}}{dt} + \frac{\partial (\rho u \vec{v})}{\partial x} - \vec{v} \frac{\partial (\rho u)}{\partial x} + \frac{\partial (\rho v \vec{v})}{\partial y} - \vec{v} \frac{\partial (\rho v)}{\partial y} + \frac{\partial (\rho w \vec{v})}{\partial z} - \vec{v} \frac{\partial (\rho w)}{\partial z}$$

MOTO CHE:
 $\frac{\partial (\rho u \vec{v})}{\partial x} = \rho u \frac{\partial \vec{v}}{\partial x} + \vec{v} \frac{\partial (\rho u)}{\partial x}$

$$= \rho \frac{d\vec{v}}{dt} + \frac{\partial (\rho u \vec{v})}{\partial x} + \frac{\partial (\rho v \vec{v})}{\partial y} + \frac{\partial (\rho w \vec{v})}{\partial z} - \vec{v} \text{div}(\rho \vec{v})$$

$$= \rho \frac{d\vec{v}}{dt} + \dots + \vec{v} \frac{\partial \rho}{\partial t}$$

$$= \frac{\partial (\rho \vec{v})}{\partial t} + \frac{\partial (\rho u \vec{v})}{\partial x} + \frac{\partial (\rho v \vec{v})}{\partial y} + \frac{\partial (\rho w \vec{v})}{\partial z} \Rightarrow \text{INTEGRANDO} \int_W \frac{\partial (\rho \vec{v})}{\partial t} dW + \int_W \frac{\partial (\rho u \vec{v})}{\partial x} dW + \dots$$

EQ DI CONTINUITÀ:
 $\rho \text{div}(\vec{v}) + \frac{\partial \rho}{\partial t} = 0 \Rightarrow \text{div}(\rho \vec{v}) = -\frac{\partial \rho}{\partial t}$

\Rightarrow TH DIVERGENCE = $\int_W \frac{\partial (\rho \vec{v})}{\partial t} dW + \int_A \rho \vec{v} (u \cos \hat{n}_x + v \cos \hat{n}_y + w \cos \hat{n}_z) dA = \frac{\partial}{\partial t} \int_W \frac{\rho \vec{v}}{\partial t} dW - \int_A \rho \vec{v} V_n dA$

③ $\int_W \frac{\phi_x}{\partial x} dW = - \int_A \phi_x \cos(\hat{n}_x) dA$

$$\Rightarrow \vec{G} - \frac{\partial}{\partial t} \int_W \rho \vec{v} dW + \int_A \rho \vec{v} V_n dA = - \int_A \vec{\phi}_n dA$$

BERNATI QUANTITÀ DI MOTO: INERTIA FLUSSO QUANTITÀ DI MOTO SUL CONTORNO SPINTE

$$\vec{G} + \vec{I} + \vec{M} + \vec{\Pi} = 0$$

Fonte d'inertez nile per mov permanente

β $\Pi = \int_A \rho \vec{v}^2 dA = \beta \rho V_m^2 A$

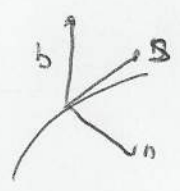
$$\beta = \frac{\int V^2 dA}{V_m^2 A}$$

① FLUIDO IDEALE $\rightarrow \mu=0 \rightarrow \tau=0 \rightarrow$ Non perde energia lungo il suo moto
 • 1° ordine
 • T cost

$$\int (\vec{F} - \vec{a}) = \text{grad}(p)$$

FORMULA DI EULERO

$$\begin{cases} \rho(f_x - a_x) = \frac{\partial p}{\partial x} \\ \rho(f_y - a_y) = \frac{\partial p}{\partial y} \\ \rho(f_z - a_z) = \frac{\partial p}{\partial z} \end{cases}$$



② FLUIDO PESANTE $\Rightarrow F = -g \text{ grad } z$

$$\begin{cases} \rho \left(-g \frac{\partial z}{\partial s} - \frac{a}{\partial s} \right) = \frac{\partial p}{\partial s} \\ \rho \left(-g \frac{\partial z}{\partial n} - \frac{a}{\partial n} \right) = \frac{\partial p}{\partial n} \\ \rho \left(-g \frac{\partial z}{\partial b} - \frac{a}{\partial b} \right) = \frac{\partial p}{\partial b} \end{cases}$$

Componente s, r e tangenziale, r e normale, r e bin

$$\Rightarrow \begin{cases} \rho \left(-g \frac{\partial z}{\partial s} - \frac{dv}{dt} \right) = \frac{\partial p}{\partial s} \\ \rho \left(-g \frac{\partial z}{\partial n} - \frac{v^2}{r} \right) = \frac{\partial p}{\partial n} \\ \rho \left(-g \frac{\partial z}{\partial b} \right) = \frac{\partial p}{\partial b} \end{cases}$$

$$\Rightarrow \begin{cases} \rho g \frac{\partial z}{\partial s} + \rho \frac{dv}{dt} = \frac{\partial p}{\partial s} = 0 \\ \rho g \frac{\partial z}{\partial n} + \rho \frac{v^2}{r} = \frac{\partial p}{\partial n} = 0 \\ \rho g \frac{\partial z}{\partial b} = \frac{\partial p}{\partial b} = 0 \end{cases}$$

③ FLUIDO INCOMPRESSIBILE
 $\rho = \text{cost}$
 $\rho g = \gamma = \text{cost}$

$$\begin{cases} \frac{\gamma}{\rho} \frac{\partial z}{\partial s} + \frac{1}{\rho} \frac{dp}{dt} - \frac{1}{\rho} \frac{\partial p}{\partial s} = 0 \\ \frac{\gamma}{\rho} \frac{\partial z}{\partial n} + \frac{1}{\rho} \frac{v^2}{r} - \frac{1}{\rho} \frac{\partial p}{\partial n} = 0 \\ \frac{\gamma}{\rho} \frac{\partial z}{\partial b} + \frac{1}{\rho} \frac{\partial p}{\partial b} = 0 \end{cases}$$

$$\Rightarrow \begin{cases} \frac{\partial}{\partial s} \left(z + \frac{p}{\gamma} \right) = -\frac{1}{g} \frac{dv}{dt} \\ \frac{\partial}{\partial n} \left(z + \frac{p}{\gamma} \right) = -\frac{1}{g} \frac{v^2}{r} \\ \frac{\partial}{\partial b} \left(z + \frac{p}{\gamma} \right) = 0 \end{cases}$$

$\rightarrow h \Delta E_p = \Delta v \sqrt{g} \left[\frac{m}{s} \frac{J}{m} \right]$
 la quale potenziale è invariante prop
 all'accelerazione centripeta
 diminuisce verso il centro di curvatura
 $\rightarrow v_a \rightarrow 0$ e
 diventa infinita
 se $r = \infty$

④ LUNGO LA DI S
 $V(t, s(t))$

$$\frac{dV}{dt} = \frac{\partial V}{\partial t} + \frac{\partial V}{\partial s} \frac{ds}{dt} = \frac{\partial V}{\partial t} + \frac{\partial V}{\partial s} V = \frac{\partial V}{\partial t} + \frac{\partial V}{\partial s} \left(\frac{V^2}{2} \right)$$

$$\frac{\partial(V^2)}{\partial s} = 2V \frac{\partial V}{\partial s}$$

$$\frac{\partial}{\partial s} \left(z + \frac{p}{\gamma} \right) = -\frac{1}{g} \frac{\partial V}{\partial t} + \frac{\partial}{\partial s} \left(\frac{V^2}{2} \right)$$

$$\frac{\partial}{\partial s} \left(z + \frac{p}{\gamma} + \frac{V^2}{2g} \right) = -\frac{1}{g} \frac{\partial V}{\partial t}$$

⑤ ISTO PERMANENTE
 $\frac{\partial V}{\partial t} = 0$

BERNOLLI

$$z + \frac{p}{\gamma} + \frac{V^2}{2g} = \text{cost}$$

1. PESANTE
2. INCOMPRESSIBILE
3. FLUIDO IDEALE
4. INCOMPRESSIBILE
5. correnti lineari o gradualmente vortice

CORRENTI IN TUBO DI FLUSSO

$$\frac{H \cdot \rho W}{\rho} = \frac{E_{me}}{\rho} \Rightarrow p = H \rho Q \quad P = \int \frac{\rho v^3}{2g} dA = \rho \alpha \left(\frac{V_m^3}{2g} \right)$$

$$P = \rho \int_A \left(z + \frac{p}{\gamma} + \frac{v^2}{2g} \right) v dA + \rho \int_A \frac{v^3}{2g} dA \Rightarrow P = \rho \left(z + \frac{p}{\gamma} \right) Q + \rho \alpha \frac{V_m^3}{2g} Q = \text{cost}$$

P cinetico

$$z + \frac{p}{\gamma} + \alpha \frac{V_m^2}{2g} = \text{cost}$$

È si conserva se $\rho = \text{cost}$
 ma è rettilinea

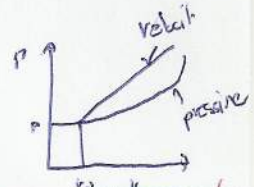
APPLICAZIONE

1) TORNAIO



$$\rho(\vec{F} - \vec{z}) = \rho \nabla \phi$$

lungo \vec{n} : $-\frac{1}{g} \frac{v^2}{r} = \frac{\rho}{\rho} \left(\frac{\rho}{g} \right) = \text{Abbiamo un n opposto - cambio segno} \rightarrow \frac{\partial}{\partial n} \left(\frac{\rho}{g} \right) = \frac{1}{g} \frac{v^2}{r}$



$$-\frac{\partial}{\partial n} \left(\frac{\rho}{g} \right) = \frac{r}{g} \frac{v^2}{h} = \int_{p_0}^p dp = \rho \int_{v_0}^v \frac{v^2}{h} \rightarrow p(r) - p_0 = \rho \frac{c_1^2 r^2}{2} \Big|_{r_0}^r$$

$$p(r) = p_0 + \frac{\rho c_1^2}{2} (r^2 - r_0^2)$$

velocità lineare ma pressione quadratiche

2) TURBO

$$\begin{cases} \frac{\partial}{\partial s} \left(\frac{\rho v}{g} \right) = -\frac{1}{g} \frac{dv}{dt} \\ \frac{\partial}{\partial s} \left(\frac{\rho v^2}{g} \right) = -\frac{1}{g} \frac{v^2}{r} \\ \frac{\partial}{\partial b} \left(\frac{\rho v}{g} \right) = 0 \end{cases}$$

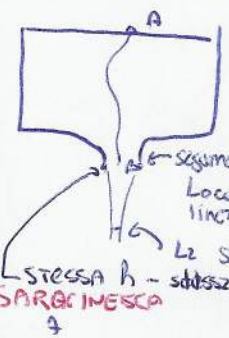
se rettilineo $r = \infty$

$$\begin{cases} \frac{\partial}{\partial s} \left(z + \frac{p}{g} \right) = \frac{1}{g} \frac{dv}{dt} \\ \frac{\partial}{\partial n} \left(z + \frac{p}{g} \right) = 0 \\ \frac{\partial}{\partial b} \left(z + \frac{p}{g} \right) = 0 \end{cases} \rightarrow \text{la pressione varia con la velocità di velocità}$$

→ PRESSIONE IDROSTATICA

PROCESSO DI EFFLUSSO

velocità turbolente



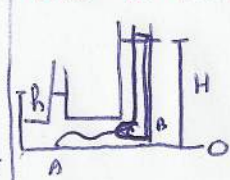
molto lento → foro piccolo
SAGOMAZIONE / CORRETTA LINEARITÀ

$$z_1 + \frac{p_1}{g} + \frac{v_1^2}{2g} = z_2 + \frac{p_2}{g} + \frac{v_2^2}{2g}$$

$$v_B^2 = 2g(z_1 - z_2) \rightarrow v_A = \sqrt{2g(z_1 - z_2)} \rightarrow v_B = C_v \sqrt{2g(z_1 - z_2)}$$

$$Q = c_d A v = A C_c C_v \sqrt{2g(z_1 - z_2)} = \mu A \sqrt{2g(z_1 - z_2)} = \varphi$$

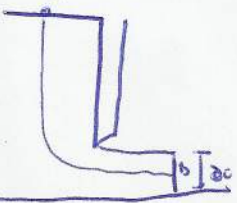
TURBO DI PITAGOR



$$z_B + \frac{p_B}{g} + \frac{v_B^2}{2g} = z_A + \frac{p_A}{g} + \frac{v_A^2}{2g} \rightarrow \text{P.T. DI RISTABILIMENTO}$$

$$h_1 + \frac{v_1^2}{2g} = H$$

$$v_1^2 = (H - h_1) 2g = \sqrt{2g \Delta h}$$



$$z_1 = z_0 + \frac{p_1}{g} + \frac{v_1^2}{2g}$$

$$\Rightarrow v_1 = \sqrt{2g(z_2 - z_0)}$$

coef. di contrazione

$$A C_c = z_c b \rightarrow z_k C_c = z_c k \rightarrow z_c = z C_c$$

$$\rho(\vec{F} - \vec{z}) = \nabla p \quad \frac{dv}{dt} = \frac{\partial v}{\partial t} + v \frac{\partial v}{\partial s}$$

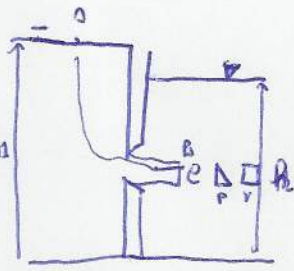
lungo s: $\rho \left(\frac{\partial v}{\partial t} + v \frac{\partial v}{\partial s} \right) = \frac{\partial p}{\partial s}$

$$g \frac{\partial z}{\partial s} - \rho \frac{dv^2}{dt} = \frac{\partial p}{\partial s}$$

$$\frac{\partial}{\partial s} \left(g z + \frac{v^2}{2} \right) + \frac{1}{\rho} \frac{\partial p}{\partial s} = 0$$

$$g z + \frac{v^2}{2} + \int \frac{dp}{\rho} = \text{cost}$$

EFFLUSSO INTERNO



$$z_1 + \frac{p_1}{g} + \frac{v_1^2}{2g} = z_2 + \frac{p_2}{g} + \frac{v_2^2}{2g}$$

$$h_1 = h_2 + \frac{v_2^2}{2g} \rightarrow v_2 = \sqrt{2g(h_1 - h_2)}$$

FLUIDO COMPRESSIBILE → Aria sotto 100 km/h è incompressibile

$$\rho v^n = \text{cost} \text{ legge dei gas} \rightarrow \rho \left(\frac{M}{p} \right)^n = \text{cost} \rightarrow \frac{\rho}{p^n} = \text{cost} \rightarrow \frac{\rho}{\text{cost}} = p^n \Rightarrow \int \frac{dp}{p} = \text{cost} \int \frac{d\rho}{p^n}$$

$$\begin{cases} n=1 & c \int \frac{d\rho}{p} = c \ln p \\ n \neq 1 & c \int \frac{d\rho}{p^n} = c \frac{p^{-n+1}}{-n+1} = \frac{n}{n-1} \frac{1}{p} p = \frac{n}{n-1} \frac{p}{\rho} \end{cases}$$

$$p = \text{cost} \rightarrow g z + \frac{v^2}{2} + \frac{p_2}{\rho} = \text{cost}$$

FLUIDI COMPRIMIBILI

$$\rho z + \frac{v^2}{2} + \int \frac{dP}{\rho} = \text{cost} \quad \begin{cases} n=1 & = c \ln p \\ n \neq 1 & = \frac{n}{n-1} \frac{p}{\rho} \end{cases}$$

5) $n \neq 1$

PISTO DI STENO



$z_1 = z_2$

PISTO DI RISTRETTO

$\rho = \text{cost}$ $\forall n$ → Bernoulli = $\rho z + \frac{P_2}{\rho} + \frac{v_2^2}{2} = \rho z + \frac{P_1}{\rho} + \frac{v_1^2}{2}$ $P_2 - P_1 = \rho \frac{v_1^2}{2} = \boxed{P_2 - P_1 = \frac{v_1^2}{2} \rho}$

$C = \text{celerità} = \text{velocità di propagazione di una perturbazione nel fluido} = \sqrt{\frac{E}{\rho}} = \text{in un fluido} = \sqrt{\frac{n P_2}{\rho}} - C_1^2 = \frac{n P_1}{\rho} \quad \frac{P_1}{\rho} = \frac{C_1^2}{n}$

$P_2 - P_1 = \rho \frac{v_1^2}{2} \Rightarrow \frac{P_2 - P_1}{P_1} = \frac{\rho v_1^2}{2 P_1} \Rightarrow \boxed{\frac{P_2 - P_1}{P_1} = \frac{n}{2} \pi_0^2}$ $\rho = \text{cost} \forall n$

$\pi_0 = \frac{v}{c}$

$n=1 \quad \rho \neq \text{cost}$

$\rho z + \frac{v^2}{2} + c \ln P_2 = \rho z + \frac{v^2}{2} + c \ln P_1 \Rightarrow \ln \frac{P_2}{P_1} = \frac{1}{2c} v_1^2$
 $\Rightarrow \ln \frac{P_2}{P_1} = \frac{1}{2} \frac{v_1^2}{c^2} \Rightarrow \boxed{\frac{P_2 - P_1}{P_1} = e^{\frac{\pi_0^2}{2}} - 1}$ $\rho \neq \text{cost} \quad n=1$

$C = \frac{P}{\rho}$
 $\pi_0 = \frac{c}{v}$

$C_1 = \sqrt{\frac{P_1}{\rho}}$
 $C_2 = C^2$

$n \neq 1 \quad \rho \neq \text{cost}$

$\frac{v_1^2}{2} + \frac{n}{n-1} \frac{P_1}{\rho_1} = \frac{n}{n-1} \frac{P_2}{\rho_2} \Rightarrow \frac{P_2}{P_1} = \frac{\rho_2}{\rho_1} + \frac{n-1}{n} \frac{v_1^2}{2} \frac{\rho_2}{P_1}$

$\boxed{\frac{P_2 - P_1}{P_1} = \left(1 + \frac{n-1}{2} \pi_0^2\right)^{\frac{n}{n-1}} - 1}$ $\rho \neq \text{cost} \quad n=1$

① $C_1^2 = \frac{P}{\rho n}$
 ② $\frac{P_1}{\rho_1^{\frac{n}{n-1}}} = \frac{P_2}{\rho_2^{\frac{n}{n-1}}}$

POTENZA CINETICA IN UN TUBO DI FLUSSO

← E per unità di peso

$H \gamma W = E$

$H \frac{\gamma W}{F} = \text{Potenza}$

$H \gamma Q = P \Rightarrow H \gamma dQ = dP \rightarrow P = \gamma \int_A \left(z + \frac{P}{\rho} + \frac{v^2}{2}\right) dQ \rightarrow \gamma \int_A \left(z + \frac{P}{\rho} + \frac{v^2}{2}\right) v dA$

→ POTENZA CINETICA = $\gamma \int \frac{v^3}{2g} dA = \alpha \int \frac{v_m^3}{2g}$ $\alpha = \frac{\int v^3 dA}{v_m^3 A}$ ← Velocità con il profilo di V

UN FLUIDO INMOVILE $\rho = \text{cost}$

$P = \gamma \int_A \left(z + \frac{P}{\rho}\right) v dA + \gamma \alpha \frac{v_m^3 A}{2g}$

$\rho \left(z + \frac{P}{\rho} + \frac{\alpha v_m^3}{2g}\right) = \text{cost}$ E si conserva
 • incompressibile
 • moto rettilineo → $\left(z + \frac{P}{\rho}\right) = \text{cost}$

③ ⇒ SI ESTENDE IL TH DI BERNOULLI PER UN TUBO DI FLUSSO (NON TRAIETTORIA)

EQUAZIONE GLOBALE PER L'EQ DINAMICO DI UN FLUIDO

$$\int_W \rho \vec{F} dW + \int_A \Phi_n dA + \int_A \rho \vec{V} v_n dA + \int_W \frac{\partial}{\partial t} (\rho \vec{V}) dW = 0$$

NON VARIA PER FLUIDI IDEALI

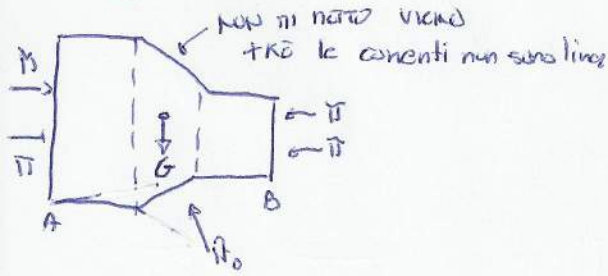


IL FLUSSO DI Q DIMIUIE NEL VANTO

NON VARIA

ESERCIZI

SPINTE DINAMICHE



$$\vec{\Pi}_1 + \vec{\Pi}_2 + \vec{G} + \vec{\Pi}_1 + \vec{\Pi}_2 + \vec{\Pi}_0 = 0$$

$$\begin{aligned} \Pi_1 &= \rho g h_1 A_1 & \Pi_1 &= \rho \vec{V} v_n A = \rho Q v_n = \rho Q v_1 \\ \Pi_2 &= \rho g h_2 A_2 & \Pi_2 &= \rho Q v_2 \end{aligned}$$

BILANCIO DI ENERGIA

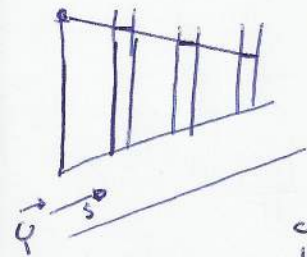
$$z_1 + \frac{p_1}{\rho} + \alpha \frac{v_{m1}^2}{2g} = z_2 + \frac{p_2}{\rho} + \alpha \frac{v_{m2}^2}{2g}$$

BILANCIO DI MASSA

$$Q_1 = Q_2 \quad v_1 A_1 = v_2 A_2$$

EQUILIBRIO $\vec{\Pi}_1 + \vec{\Pi}_2 + \vec{\Pi}_1 + \vec{\Pi}_2 + \vec{G} = 0$

FLUIDI REALI



$H \neq \text{cost} \rightarrow$ viscosità $\rightarrow \tau \rightarrow$ calore

Ha una perdita di E per unità di peso e lunghezza $= J$

VARIAZIONE di E di peso lungo $S \rightarrow \frac{dH}{ds} = -J \rightarrow \int_1^2 dH = \int_1^2 -J ds \rightarrow H_2 - H_1 = -JL \quad H_2 = H_1 - \overbrace{JL}^{\text{CARICHE PERDITE}}$

REALE $\rightarrow H_2 = H_1 - JL - \sum \Delta H$ RESTRISSIONI ETC...

TEOREMA Π

DATA UNA FUNZIONE con $n+1$ VARIABILI } una base di K elementi.
Adimensionalizzando posso ridurre a $n+1-K$ incognite

$$G = f \left(\underbrace{\rho, \theta, \nu}_{\text{GEN}}, \underbrace{\rho, \mu, \epsilon, S}_{\text{FLUIDO}}, \underbrace{v, a}_{\text{CINEMATI}}, \underbrace{t, x, g, \vec{F}}_{\text{tempo spazio forze}} \right)$$

coef geom fluido, rugosità, comprimibilità, tensione superf

SCELTO LA BASE $\begin{cases} L \rightarrow$ lunghezza $\begin{cases} M \rightarrow \rho \rightarrow$ centrale nei moti turbolenti $\begin{cases} t \rightarrow v \rightarrow$ presente nei moti stazionari

$$\Pi_6 = f \left(\gamma, \theta, \frac{v}{g}, 1, Re, Ma, We, \tau, \frac{\alpha \lambda}{r_2}, St, \frac{x}{g}, Fr, \vec{\Pi}_F \right)$$

NUMERI ADIMENSIONALI

Reynolds $[N]$ $\frac{kg}{sm}$

[EFFETTI VISCOSI]

$$\mu = [M][L^{-1}][T^{-1}]$$

$$kg \frac{m}{s^2} \frac{s}{m^2}$$

$$N = \rho^\alpha \lambda^\beta v^\gamma = M L^{-1} T^{-1} = [M L^{-3}]^\alpha [L]^\beta [M L T^{-1}]^\gamma$$

FORCE INERZIALI
FORTE VISCOSI

$$\begin{cases} \alpha = 1 \\ -3\alpha + \beta + \gamma = -1 \\ -\gamma = -1 \end{cases} \rightarrow \begin{cases} \alpha = 1 \\ \beta = 1 \\ \gamma = 1 \end{cases}$$

$$\dot{N} = \frac{N}{\rho v \lambda}$$

$$\Rightarrow Re = \frac{\rho v \lambda}{\mu}$$

Grashof $[E]$ $\frac{kg}{ms^2}$

$$dp = \epsilon \frac{dw}{x} \rightarrow [N][L^{-2}][1][L][T^{-2}][L^2]$$

[FLUIDI COMPRESSIBILI]

$$[E] = [M]^\alpha [L^{-1}]^\beta [T^{-2}]^\gamma = \rho^\alpha \lambda^\beta v^\gamma = [M L^{-3}]^\alpha [L]^\beta [L T^{-1}]^\gamma$$

$$\begin{cases} \alpha = 1 \\ -3\alpha + \beta + \gamma = -1 \\ -\gamma = -2 \end{cases} \rightarrow \begin{cases} \alpha = 1 \\ \beta = 0 \\ \gamma = 2 \end{cases}$$

$$\dot{E} = \frac{E}{\rho v^2}$$

$$Ca = \frac{\rho v^2}{E}$$

$$Ca = \frac{\rho v^2}{E} = \frac{v^2}{\frac{E}{\rho}} = \frac{v^2}{c^2} = \Pi_2^2$$

WEBER $[S]$ $\frac{kg}{m^2}$

[SE HO + FLUIDI, CURVATURA, TENSIONE superficiale]

$$\begin{cases} \alpha = 1 \\ -3\alpha + \beta + \gamma = 0 \\ -\gamma = -2 \end{cases} \rightarrow \begin{cases} \alpha = 1 \\ \beta = 1 \\ \gamma = 2 \end{cases}$$

$$We = \frac{S}{\rho v^2} = \frac{\rho v^2}{\frac{S}{\rho}}$$

← SFORZO TURBOLINIZANTE

← SFORZO DI TENSIONE SUP

$\dot{a} = [L][T]^{-2}$

[NUMI NON STAZIONARI]

$$\begin{cases} \alpha = 0 \\ \beta = -1 \\ \gamma = 2 \end{cases} \quad \dot{a} = \frac{a \lambda}{v^2}$$

STROUHAL $[T]$

[NUMI NON STAZIONARI]

$[T] = I$

$$\begin{cases} \alpha = 0 \\ \beta = 1 \\ \gamma = 1 \end{cases}$$

$$St = \frac{l}{v t} = \frac{l}{v} \left(\frac{1}{t} \right)$$

tempo medio di percorso
t è tempo che studia

FRUD $[F]$

$$\dot{g} = \frac{g \lambda}{v^2}$$

$$Fr^2 = \frac{v^2}{g \lambda} \frac{\rho}{\rho}$$

SFORZI DI INERZIA TURBOLINIZANTI
SFORZI PER INERZIA RESO

[SOLO SE HO + FLUIDI CHE LA GRAVITÀ DA ITERAZIONI DIFFERENTI]

SIMILITUDINI

- Geometrica $\frac{L'}{L} = cost = \lambda_L$
- Cinematica $\frac{v'}{v} = cost = \lambda_v$ $\frac{\omega'}{\omega} = cost = \lambda_\omega$ $\frac{T'}{T} = \frac{v' L'}{L v} = \frac{\lambda_L}{\lambda_v}$
- Dinamica $\frac{F'}{F} = cost = \dots$

CONDIZIONE SUFF. ① $\frac{F'}{F} = \lambda_F \Rightarrow \frac{m' a'}{m a} = \frac{\rho' \omega'}{\rho \omega} \lambda_a = \lambda_\rho \lambda_\omega^3 \lambda_a = \lambda_\rho \lambda_L^3 \lambda_v^2$

② TUTTI I PARAMETRI DI CONTROLLO SONO SIMILI

SIMILITUDINI PARZIALI PER CUI COINCIDONO LE VARIABILI BASE DEL SISTEMA AUTOSIMILE

SLIDE

MODELLI FLUIDODINAMICI

$$G = f(R_e, M_z, W_e, F_r, \theta, \frac{v}{\alpha}, \frac{\rho \ell}{\nu}, \frac{x}{L}, \frac{y}{L}, \frac{z}{L}, St)$$

- 1) ESCALA geom
- 2) ACC. gravit
- 3) FLUIDO

$$\begin{aligned} \frac{L'}{L} &= \lambda_L = \lambda \\ \frac{g'}{g} &= 1 = \lambda_g \rightarrow \text{sono sulla terra} \\ \frac{\rho'}{\rho} &= \lambda_\rho = 1 \\ \frac{\mu'}{\mu} &= \lambda_\mu = 1 \rightarrow \text{Non cambio il fluido} \\ \frac{\epsilon'}{\epsilon} &= \lambda_\epsilon = 1 \\ \frac{s'}{s} &= \lambda_s = 1 \end{aligned}$$

6 VINCOLI per 3 GDL

Modello in similitudine di Reynold

$$Re' = Re \Rightarrow \lambda_{Re} = 1 \quad \frac{\rho v \ell}{\mu} = 1 \quad \frac{v'}{v} = \frac{\ell}{\ell'} = \lambda_v = \frac{1}{\lambda_L}$$

$$M_z' = M_z \quad \frac{v'}{c'} = \frac{v}{c} \Rightarrow \frac{v'}{\sqrt{\frac{\epsilon'}{\rho'}}} = \frac{v}{\sqrt{\frac{\epsilon}{\rho}}} \Rightarrow \lambda_v = 1$$

Se $\lambda_v = 1 \Rightarrow \lambda_L = 1$
 m2 $\lambda_L = \lambda \neq 1$

SIMILITUDINE INCOMPRESSIBILE

SIMILITUDINE DI REYNOLDS

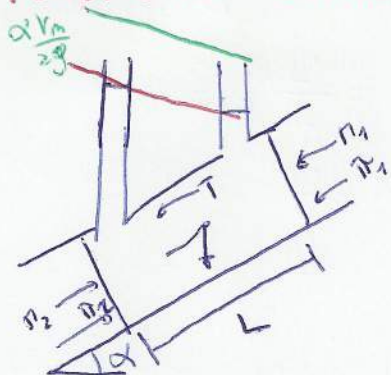
$$\lambda_{Re} = 1 \Rightarrow \lambda_v = \frac{1}{\lambda_L} \quad \text{se puzo } \lambda_L = \frac{1}{10} \quad \lambda_v = \frac{1}{10} \neq 1$$

$$\frac{\lambda_L}{\lambda_v} = \lambda_T = \frac{1}{100} \quad \lambda_a = \frac{\lambda_\omega^3}{\lambda_L} = \frac{1^3}{10} = \frac{1}{1000}$$

$$\lambda_F = \frac{m' a'}{m a} = \frac{\rho' L^3 a'}{\rho L^3 a} = 1 \quad \lambda_L^3 \lambda_a = 1 \Rightarrow \text{SIMILITUDINE DI REYNOLDS STASSE FORTE}$$

$\lambda_{Ma} = \frac{v'}{\epsilon'} \frac{\epsilon}{s} = \frac{1}{\lambda_L} \rightarrow$ il mio modello è un M2 10 volte sup \rightarrow NON BENE

PERDITE DI CARICO IN PROBLEMI MONO-DIMENSIONALI



$$\frac{\partial H}{\partial s} = -\zeta$$

$$\zeta = f(D, \nu, v, \rho, \mu, \epsilon, \delta, r, \alpha, \gamma, \beta, \vec{F})$$

per unità di lunghezza

NO T SUP
NO ACC
1 FLUIDO
NO FURTO

NUM DI REE della posizione STAZIONARIA

BASE

- LAM (ρ, ν, D) ②
- TURB (ρ, ν, D) ①

$$\textcircled{1} \frac{\zeta}{\rho v^2} = f_1\left(1, \frac{\nu}{D}, 1, Re, 1\right)$$

$$\textcircled{2} \frac{\zeta}{\rho v^2} = f_2\left(1, \frac{\nu}{D}, Re, 1, 1\right)$$

LUNGO S

$$\vec{\pi}_1 + \vec{\pi}_2 + \vec{\pi}_1 + \vec{\pi}_2 + \vec{T} + \vec{W} = 0$$

$$p_1 A - p_2 A + \gamma W \sin \alpha - |\vec{T}| = 0$$

$$p_1 A \pi - p_2 A \pi + \gamma A (z_2 - z_1) - |\vec{T}| = 0$$

$$\vec{T} = A \gamma \left[\left(\frac{p_1}{\gamma} + z_1 \right) - \left(\frac{p_2}{\gamma} + z_2 \right) \right]$$

$$\vec{T} = A \gamma L \zeta$$

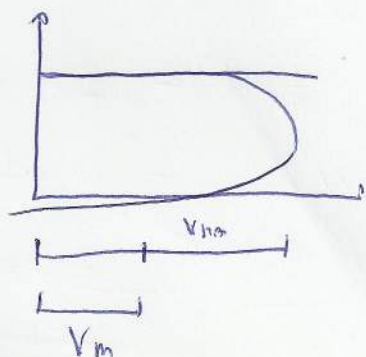
$$\zeta = \frac{|\vec{T}|}{A L \gamma} = \frac{\gamma \pi D \lambda}{\gamma A \lambda} = \frac{\gamma \pi D \lambda}{\gamma \pi \frac{D^2}{4}} = \frac{4 \lambda}{D}$$

PER TUTTI I CASI

$$\zeta = \begin{cases} \frac{4 \lambda}{D} \stackrel{\text{LAM}}{=} \frac{4}{D} \rho \nu^2 f\left(\frac{\nu}{D}, Re\right) = \frac{\lambda_{\text{TURBOLATO}}}{D} f_1\left(Re, \frac{\nu}{D}\right) \frac{v^2}{2gD} \\ \frac{4 \lambda}{D} \stackrel{\text{TURB}}{=} \frac{4}{D} \frac{\rho v^2}{D} f\left(\frac{\nu}{D}, Re\right) = \frac{\lambda_{\text{LAMINARE}}}{Re} f_2\left(Re, \frac{\nu}{D}\right) \frac{v^2}{2gD} \end{cases}$$

α e β nel moto laminare

$$\alpha = \frac{\int_0^R v^3 dA}{v_m^3 A} = \frac{28}{4} \frac{v_m^3 A}{v_m^3 A} = 2$$

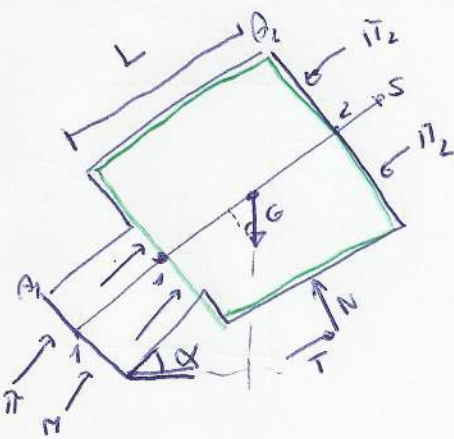


$$\beta = \frac{\int v^2 dA}{v_m^2 A}$$

$$\beta = \frac{4}{3} \frac{v_m^3 A}{v_m^2 A} = \frac{4}{3}$$

PERDITE LOCALI

BRUSCO ALLARGAMENTO



$$\vec{M}_1 + \vec{N}_1 + \vec{N}_2 + \vec{M}_2 + \vec{G} + \vec{T} + \vec{N} = 0$$

$$M_1 + N_1 - M_2 - N_2 - G \sin \alpha + T = 0$$

$$\rho Q V_1 + p_1 A_1 + \rho Q V_2 - p_2 A_2 - \gamma A_2 L \sin \alpha + T = 0$$

TRASMISSIVE

$$\rho Q (V_1 - V_2) + p_1 A_1 - p_2 A_2 - \gamma A_2 (z_2 - z_1) = 0$$

$$\rho Q (V_1 - V_2) + A_2 [p_1 - p_2 - \gamma (z_2 - z_1)] = 0$$

$$\rho Q (V_1 - V_2) = \gamma A_2 \left[-\frac{p_1}{\gamma} + z_1 + \frac{p_2}{\gamma} + z_2 \right]$$

$$\rho Q (V_1 - V_2) = \gamma A_2 \left[\left(\frac{p_2}{\gamma} + z_2 \right) - \left(\frac{p_1}{\gamma} + z_1 \right) \right]$$

LA LINEA PIEZOMETRICA NON STA TANTO

$$\Delta H = z_1 + \frac{p_1}{\gamma} + \frac{v_1^2}{2g} = z_2 + \frac{p_2}{\gamma} + \frac{v_2^2}{2g}$$

$$\Delta H = \left(z_1 + \frac{p_1}{\gamma} \right) - \left(z_2 + \frac{p_2}{\gamma} \right) + \frac{1}{2g} (v_1^2 - v_2^2)$$

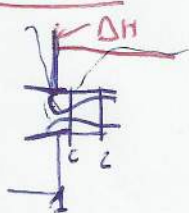
$$\Delta H = \frac{\rho Q (V_1 - V_2)}{\gamma A_2} + \frac{1}{2g} (v_1^2 - v_2^2) \rightarrow \frac{v_2 (v_1 - v_2)}{g} + \frac{1}{2g} (v_1^2 - v_2^2) = \Delta H$$

$$\Delta H = \frac{1}{2g} (2 v_2 v_1 + 2 v_2^2 + v_1^2 - v_2^2) = \frac{1}{2g} (v_1 - v_2)^2$$

coef.

CASO PARTICOLARE: ingresso subacqueo
 $\frac{1}{2g} (v_1 - 0)^2 \Rightarrow$ Perda tutta il termine cinetico

INBOCO



$$\Delta H_{C1} = \frac{v_1^2}{2g} \approx 0,1 \frac{v_1^2}{2g}$$

$$Q_1 = Q_2 \rightarrow V_1 A_1 = V_2 A_2 \rightarrow V_2 = V_1 \frac{A_1}{A_2} = V_1 \frac{D_1^2}{D_2^2}$$

$V_2 = \frac{V_1}{C_c}$

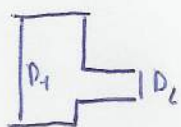
$$\Delta H_{C2} = \frac{1}{2g} (V_2 - v_1)^2$$

$$\rightarrow \frac{v_1^2}{2g} \left(\frac{v_1}{V} - 1 \right)^2$$

$$\rightarrow \Delta H_{C2} = \frac{v_1^2}{2g} \left(\frac{1}{C_c} - 1 \right)^2 \approx 0,5 \frac{v_1^2}{2g}$$

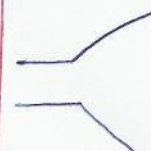
$$\Delta H = \Delta H_{C1} + \Delta H_{C2} = \frac{1}{2} \frac{v_1^2}{2g}$$

BRUSCO RESTRINGIMENTO



$$\Delta H = \frac{n v_1^2}{2g} \quad n = 0,5 \quad D_1 > 2 D_2$$

DIV



$$\Delta H = m(\beta) \frac{1}{2g} (v_1 - v_2)^2$$

BARACINESCA



$$\Delta H = \frac{1}{2g} (V_2 - v_1)^2$$

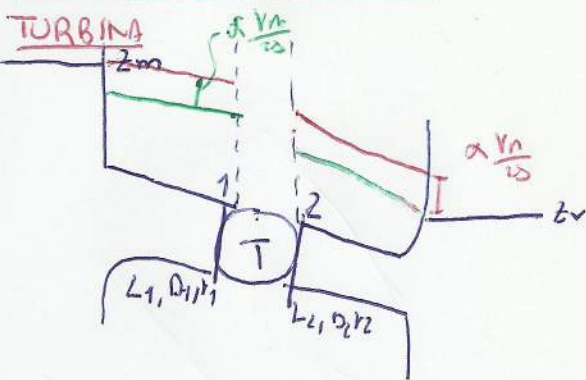
$$Q_e = Q_u$$

$$V_1 A_1 = V_2 A_2 \rightarrow V_2 = \frac{V_1 A_1}{A_2}$$

$$V_2 = \frac{V_1 A_1}{A_2} = \frac{V_1}{C_m}$$

MACCHINE IDRAULICHE

TURBINA



LA TURBINA È "STUDIABILE" COME UNA PERDITA
È VIENE ceduta alla turbina del fluido

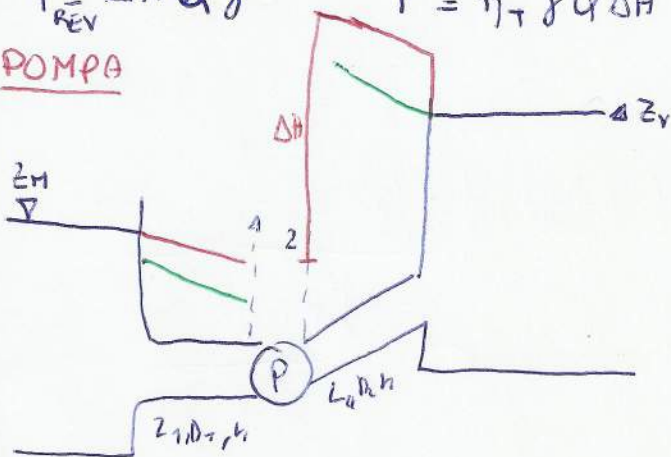
$$L_T = \Delta H = H_1 - H_2 = z_m - \sum L_1 - (z_v + \sum L_2 + \alpha \frac{V_2^2}{2g})$$

$$L_T = z_m - \sum L_1 - z_v - \sum L_2 - \alpha \frac{V_2^2}{2g} \quad \leftarrow \begin{matrix} \text{SALTO GEODETICO} \\ (z_m - z_v) \end{matrix} - \begin{matrix} \text{PERDITE} \\ (\sum L_1 + \sum L_2 + \alpha \frac{V_2^2}{2g}) \end{matrix}$$

$$P_{REV} = \Delta H Q \gamma$$

$$P = \eta_T \gamma Q \Delta H$$

POMPA



$$\Delta H = H_2 - H_1$$

$$\Delta H = -(z_m + \sum L_1) + (z_v + \sum L_2 + \alpha \frac{V_2^2}{2g})$$

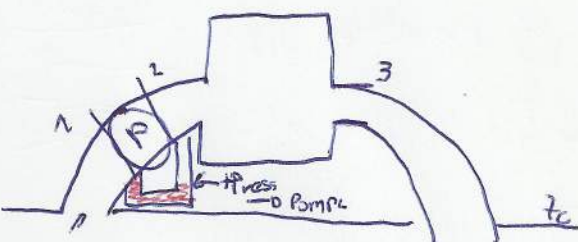
$$\Delta H = (z_v - z_m) + (\sum L_1 + \sum L_2 + \alpha \frac{V_2^2}{2g})$$

FORNIRE per il salto geodetico + tutte le perdite

$$P_{rev} = \gamma Q \Delta H$$

$$P = \frac{\gamma Q \Delta H}{\eta_P}$$

CIRCUITO CHIUSO



$$H_1 = z_c - \sum L_1 - 1,16 \frac{V^3}{2g}$$

$$H_3 = z_c + \sum L_3 + \alpha \frac{V^3}{2g} + \frac{1}{2} \frac{V^2}{2g}$$

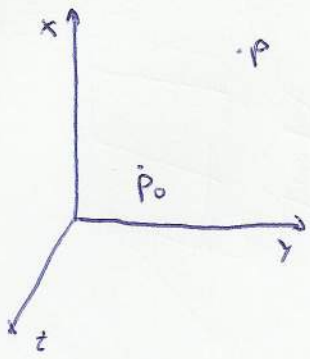
$$H_2 = H_3 + \sum L_2 + \alpha \frac{V_2^2}{2g}$$

$$\Delta H = H_2 - H_1 = z_c + \sum L_3 + \alpha \frac{V^2}{2g} + \frac{V^2}{4g} + \sum L_2 + \alpha \frac{V_2^2}{2g} - z_c + \sum L_1 + 1,16 \frac{V^2}{2g}$$

$$\sum (L_1 + L_2 + L_3) + \frac{V^2}{2g} (\alpha + 0,5 + \alpha + 1,16)$$

DEVO FURNIRE E SUO PER UNCONO
LE PERDITE

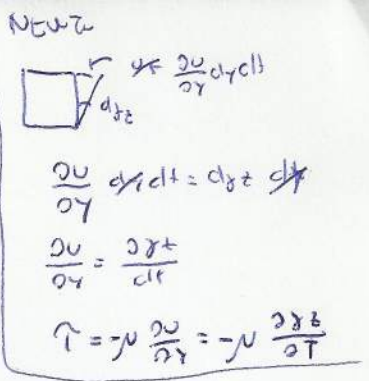
DEFORMAZIONI



$$\vec{V}(P_0) = \vec{U}_0 + \vec{v}_0 + \vec{z}_0$$

$$\vec{V}(P) = \vec{U}_0 + \frac{\partial \vec{V}_0}{\partial x} dx + \frac{\partial \vec{V}_0}{\partial y} dy + \frac{\partial \vec{V}_0}{\partial z} dz$$

$$\begin{cases} U_x = U_0 + \frac{\partial U}{\partial x} dx + \frac{\partial U}{\partial y} dy + \frac{\partial U}{\partial z} dz \\ V = V_0 + \frac{\partial V}{\partial x} dx + \frac{\partial V}{\partial y} dy + \frac{\partial V}{\partial z} dz \\ W = W_0 + \frac{\partial W}{\partial x} dx + \frac{\partial W}{\partial y} dy + \frac{\partial W}{\partial z} dz \end{cases}$$



$$\vec{V} = \begin{bmatrix} U \\ V \\ W \end{bmatrix} \quad \vec{V}_0 = \begin{bmatrix} U_0 \\ V_0 \\ W_0 \end{bmatrix} \quad d\vec{x} = \begin{bmatrix} dx \\ dy \\ dz \end{bmatrix}$$

$$\bar{D} = \begin{bmatrix} \frac{\partial U}{\partial x} & \frac{\partial U}{\partial y} & \frac{\partial U}{\partial z} \\ \frac{\partial V}{\partial x} & \frac{\partial V}{\partial y} & \frac{\partial V}{\partial z} \\ \frac{\partial W}{\partial x} & \frac{\partial W}{\partial y} & \frac{\partial W}{\partial z} \end{bmatrix}$$

$$\vec{V} = \vec{V}_0 + \bar{A} d\vec{x}$$

$$\bar{A} = \frac{\bar{A} + \bar{A}^T}{2} + \frac{\bar{A} - \bar{A}^T}{2} = \bar{D} + \bar{R}$$

$$\bar{A}_T = \begin{bmatrix} \frac{\partial U}{\partial x} & \frac{\partial V}{\partial x} & \frac{\partial W}{\partial x} \\ \frac{\partial U}{\partial y} & \frac{\partial V}{\partial y} & \frac{\partial W}{\partial y} \\ \frac{\partial U}{\partial z} & \frac{\partial V}{\partial z} & \frac{\partial W}{\partial z} \end{bmatrix}$$

$$\bar{R} = \begin{bmatrix} 0 & \frac{1}{2} \left(\frac{\partial V}{\partial x} - \frac{\partial U}{\partial y} \right) & \dots \\ 0 & 0 & \dots \\ \dots & \dots & 0 \end{bmatrix}$$

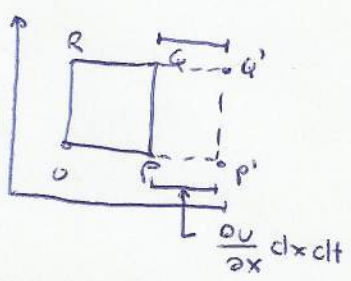
MATRICE ROTAZIONI

MATRICE DEFORMI

$$\bar{D} = \begin{bmatrix} \frac{\partial U}{\partial x} & \frac{1}{2} \left(\frac{\partial U}{\partial y} + \frac{\partial V}{\partial x} \right) & \frac{1}{2} \left(\frac{\partial U}{\partial z} + \frac{\partial W}{\partial x} \right) \\ & \frac{\partial V}{\partial y} & \dots \\ & & \frac{\partial W}{\partial z} \end{bmatrix}$$

MATRICE DI DEF [D]

DIAGONALE



$$\begin{aligned} V_0 &= 0 \quad U_0 = 0 \quad V_0 = 0 \\ V_0 &\Rightarrow U_p = \frac{\partial U}{\partial x} dx \quad V_p = \frac{\partial V}{\partial x} dx \\ V_R &\Rightarrow U_R = \frac{\partial U}{\partial y} dy \quad V_R = \frac{\partial V}{\partial y} dy \\ V_{q=0} &= U_q = \frac{\partial U}{\partial x} dx + \frac{\partial U}{\partial y} dy \quad V_q = \frac{\partial V}{\partial x} dx + \frac{\partial V}{\partial y} dy \end{aligned}$$

$$dE_x = \frac{OP'}{OP^0} = \frac{\frac{\partial U}{\partial x} dx + dt}{dx} = \frac{\partial U}{\partial x} dt$$

$$\frac{dE_x}{dt} = \frac{\partial U}{\partial x}$$

IL PRIMO TERMINE MI DEFINISCE LA VELOCITA' DI DEFORMAZIONE CASO X

ANALOGO AL TRG DIC

$$dW = W_F - W_I = \left(dx + \frac{\partial U}{\partial x} dx dt \right) \cdot \left(dy + \frac{\partial V}{\partial y} dy dt \right) \cdot \left(dz + \frac{\partial W}{\partial z} dz dt \right) - dx dy dz$$

$$\frac{dW}{W} = \frac{\partial U}{\partial x} dt + \frac{\partial V}{\partial y} dt + \frac{\partial W}{\partial z} dt$$

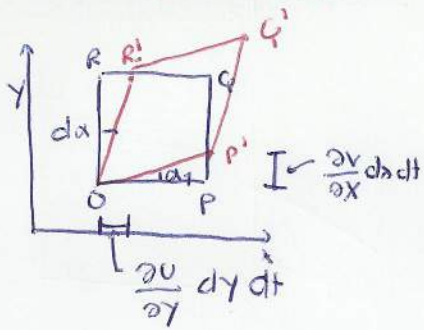
$$\frac{1}{W} \frac{dW}{dt} = \text{div}(\vec{V})$$

IL PRIMO TERMINE E' LA VELOCITA' DI DEF DI VOLUME UNITARIO SE $\rho=0$ $\text{div}(\vec{V})=0$

Nell'eq di continuita

$$\frac{d\rho}{dt} + \rho \text{div}(\vec{V}) = \frac{d\rho}{dt} + \frac{\rho}{W} \frac{dW}{dt} = 0$$

TERMINI EXTRADIAGONALI



$$\frac{1}{2} \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right)$$

$$\frac{\partial u}{\partial y} dx dt = dx \tan(\alpha)$$

$$\frac{\partial v}{\partial x} dx dt = dx \tan(\alpha)$$

$$\left[\frac{\partial u}{\partial y} = \frac{d\alpha}{dt} \right]$$

$$\left[\frac{\partial v}{\partial x} = \frac{d\alpha}{dt} \right]$$

→ VOLUME IDENTICO VARIAZIONE DI FORMA MA DI VOLUME

$dx_1 dx_2 = d\delta_z$ Giace sul piano zeta

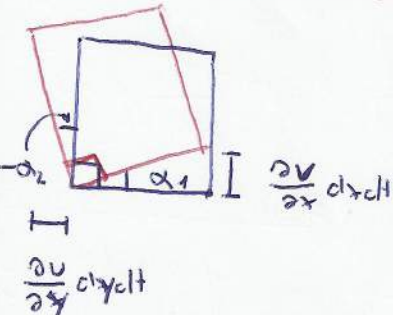
$$d\delta_z = \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) dt \rightarrow \frac{d\delta_z}{dt} = \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x}$$

$$\underline{\underline{D}} = \begin{bmatrix} \frac{d\epsilon_x}{dt} & \frac{1}{2} \frac{d\gamma_{xy}}{dt} & \frac{1}{2} \frac{d\gamma_{xz}}{dt} \\ \text{"} & \frac{d\epsilon_y}{dt} & \frac{1}{2} \frac{d\gamma_{xy}}{dt} \\ \text{"} & \text{"} & \frac{d\epsilon_z}{dt} \end{bmatrix}$$

$$\tau = \mu \frac{\partial u}{\partial y}$$

Le componenti di D mi indicano metà delle velocità di deformazione

MATRICE DI ROTAZIONE [A] → NO DEFORMAZIONE



$$\text{media: } \frac{\alpha_1 + (-\alpha_2)}{2}$$

$$= \frac{1}{2} \left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right) dt$$

$$\Rightarrow \left[\frac{1}{2} \left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right) = \frac{1}{2} \frac{(d\alpha_1 - d\alpha_2)}{dt} \right]$$

↑
velocità medie di rotazione

→ Se $dx_1 = dx_2$ zvv una rotazione rigida!

$$\underline{\underline{D}} = \begin{bmatrix} 0 & \omega_z & \omega_y \\ -\text{"} & 0 & \omega_x \\ -\text{"} & -\text{"} & 0 \end{bmatrix} \text{ emissione}$$

$$\bar{\omega} = \omega_x \bar{i} + \omega_y \bar{j} + \omega_z \bar{k}$$

SI SA CHE COME $\bar{\omega} = \frac{1}{2} \text{rot}(\bar{v})$

$$\begin{bmatrix} \bar{i} & \bar{j} & \bar{k} \\ \frac{\partial v}{\partial x} & \frac{\partial v}{\partial y} & \frac{\partial v}{\partial z} \\ u & v & w \end{bmatrix} = \left(\frac{\partial v}{\partial y} - \frac{\partial v}{\partial z} \right) \bar{i} - \left(\frac{\partial w}{\partial x} - \frac{\partial w}{\partial z} \right) \bar{j} + \left(\frac{\partial w}{\partial x} - \frac{\partial u}{\partial y} \right) \bar{k}$$

FLUIDI DI STOKES

FLUIDI SENZA MEMORIA, LO SFORZO DIPENDE SOLO DALLA VELOCITÀ DI DEF.

$$\underline{\underline{\phi}} = f(\underline{\underline{D}}) \text{ matrici simmetriche}$$

→ Si può dimostrare che esiste sempre un sist di riferimento per cui ho matrici diagonali.

$$\begin{bmatrix} \sigma_x & 0 & 0 \\ 0 & \sigma_y & 0 \\ 0 & 0 & \sigma_z \end{bmatrix} = f \begin{bmatrix} D_{xx} & 0 & 0 \\ 0 & D_{yy} & 0 \\ 0 & 0 & D_{zz} \end{bmatrix} \quad \text{inoltre} \quad \begin{bmatrix} \sigma_x & 0 & 0 \\ 0 & \sigma_y & 0 \\ 0 & 0 & \sigma_z \end{bmatrix} = \underbrace{\begin{bmatrix} p & 0 & 0 \\ 0 & p & 0 \\ 0 & 0 & p \end{bmatrix}}_{\text{PARTE STATICA VAR DI VOL}} + \underbrace{\begin{bmatrix} \sigma_x - p & 0 & 0 \\ 0 & \sigma_y - p & 0 \\ 0 & 0 & \sigma_z - p \end{bmatrix}}_{\text{PARTE DEVIATORICA DEFORMAZIONI}}$$

In un FLUIDO NEWTONIANO ABBIAMO UN LEGAME LINEARE TRA $\underline{\underline{\sigma}}$ e $\underline{\underline{D}}$

$$\begin{cases} \sigma_x = p = \mu_{xx} D_{xx} + \mu_{yy} D_{yy} + \mu_{zz} D_{zz} \\ \sigma_y = p = \mu_{yx} D_{xx} + \mu_{yy} D_{yy} + \mu_{yz} D_{zz} \\ \sigma_z = p = \mu_{zx} D_{xx} + \mu_{zy} D_{yy} + \mu_{zz} D_{zz} \end{cases}$$

Si dimostra che $\mu_{ii} = a$ $\mu_{ij} = b$

$$\rightarrow \begin{cases} \sigma_x - p = a D_{xx} + b (D_{yy} + D_{zz}) + b D_{xx} - b D_{xx} \\ \sigma_y - p = a D_{yy} + b (D_{xx} + D_{zz}) + b D_{yy} - b D_{zz} \\ \sigma_z - p = a D_{zz} + b (D_{xx} + D_{yy}) + b D_{zz} - b D_{xx} \end{cases} \Rightarrow \begin{cases} \sigma_x - p = (a-b) D_{xx} + b \operatorname{div}(\vec{v}) \\ \sigma_y - p = (a-b) D_{yy} + b \operatorname{div}(\vec{v}) \\ \sigma_z - p = (a-b) D_{zz} + b \operatorname{div}(\vec{v}) \end{cases}$$

summato $\sigma_x + \sigma_y + \sigma_z = 3p = (a-b) \operatorname{div}(\vec{v}) + 3b \operatorname{div}(\vec{v}) \rightarrow \operatorname{div}(\vec{v}) (a-b+3b) = 0$

$\left. \begin{array}{l} \operatorname{div}(\vec{v}) = 0 \text{ fluidi incompr} \\ a=3b \end{array} \right\}$

$$\underline{\underline{\phi}} = p - 3b \underline{\underline{D}} + p \underline{\underline{I}} + b \operatorname{div}(\vec{v}) \underline{\underline{I}}$$

$$\underline{\underline{\phi}}_{xy} = \tau_{xz} = -3b \frac{1}{2} \frac{d\gamma_t}{dt} + p + b \operatorname{div}(\vec{v}) \quad \underline{\underline{I}} \rightarrow \text{ho solo termini diag } \begin{bmatrix} 1 & 0 & 0 \\ 0 & 1 & 0 \\ 0 & 0 & 1 \end{bmatrix}$$

$$\tau_{xz} = -\mu 3b \frac{1}{2} \frac{d\gamma_t}{dt} \quad \rightarrow \quad 3b \frac{1}{2} = \mu \quad b = \frac{2}{3} \mu$$

$$\tau_{xz} = -\mu \frac{d\gamma_t}{dt}$$

$$\underline{\underline{\phi}} = -2\mu \underline{\underline{D}} + \left(p + \frac{2}{3} \mu \operatorname{div}(\vec{v}) \right) \underline{\underline{I}}$$

EQUAZIONI

$$\rho(\vec{P}-\vec{z}) = \text{div}(\underline{\underline{\phi}})$$

$$\left\{ \begin{aligned} \frac{d\rho}{dt} + \rho \text{div}(\vec{v}) &= 0 \end{aligned} \right.$$

$$\underline{\underline{\phi}} = \left(\rho + \frac{2}{3}\mu \text{div}(\vec{v}) \right) \underline{\underline{I}} - 2\mu \underline{\underline{D}}$$

$$\left\{ \begin{aligned} \rho &= \rho(p) \\ \text{C.C.} \end{aligned} \right.$$

1 e 3
 \Rightarrow
 lungo x

$$\rho(\vec{P}-\vec{z}_x) = \frac{\partial \rho_x}{\partial x} + \frac{\partial \tau_x}{\partial y} + \frac{\partial \pi_x}{\partial z}$$

$$\phi_x = \rho + \frac{2}{3}\mu \text{div}(\vec{v}) - 2\mu \frac{\partial u}{\partial x}$$

$$\tau_x = -2\mu \frac{1}{2} \left(\frac{\partial v}{\partial y} + \frac{\partial v}{\partial y} \right)$$

$$\pi_x = -2\mu \frac{1}{2} \left(\frac{\partial u}{\partial z} + \frac{\partial w}{\partial x} \right)$$

SOSTITUISCO $\xrightarrow{\text{lungo x}}$

$$\rho(f_x - a_x) = \frac{\partial \rho}{\partial x} + \frac{2}{3}\mu \frac{\text{div}(\vec{v})}{\partial x} - 2\mu \frac{\partial^2 u}{\partial x^2} - \mu \left(\frac{\partial^2 v}{\partial y^2} + \frac{\partial v}{\partial x \partial y} + \frac{\partial^2 u}{\partial z^2} + \frac{\partial w}{\partial x \partial z} \right)$$

$-\frac{1}{3}\mu \frac{\text{div}(\vec{v})}{\partial x}$ $+\mu \frac{\text{div}(\vec{v})}{\partial x}$ $\mu \nabla^2 u$

$$\rho(f_x - a_x) = \frac{\partial \rho}{\partial x} - \frac{1}{3}\mu \frac{\text{div}(\vec{v})}{\partial x} - \mu \nabla^2 u$$

$$\rho(f_y - a_y) = \frac{\partial \rho}{\partial y} - \frac{1}{3}\mu \frac{\text{div}(\vec{v})}{\partial y} - \mu \nabla^2 v$$

$$\rho(f_z - a_z) = \frac{\partial \rho}{\partial z} - \frac{1}{3}\mu \frac{\text{div}(\vec{v})}{\partial z} - \mu \nabla^2 z$$

LEGGE DEL MOTO

$$\rho(\vec{P}-\vec{z}) = \text{grad}(\rho) - \frac{1}{3}\mu \text{grad}(\text{div}(\vec{v})) - \mu \nabla^2 \vec{v}$$

EQUAZIONE DI NAVIER-STOKES: $\vec{\sigma}$ la legge del moto di un fluido newtoniano, incomprimibile e primo ordine

$$\left\{ \begin{aligned} \frac{d\rho}{dt} + \rho \text{div}(\vec{v}) &= 0 & \text{se } \rho = \text{cost} & \text{div}(\vec{v}) = 0 & \text{CONTINUITÀ } 1 \end{aligned} \right.$$

$$\rho(\vec{P}-\vec{z}) = \text{grad}(\rho) - \frac{1}{3}\mu \text{grad}(\text{div}(\vec{v})) - \mu \nabla^2 \vec{v}$$

$\rho = \rho(p)$ C.C.

3
 $\frac{\rho}{\rho_0}$ (u, v, w, p)

$$\rho(\vec{P}-\vec{z}) = \text{grad}(\rho) - \mu \nabla^2 \vec{v} \quad \vec{a} = -\frac{1}{\rho} \text{grad}(\rho) + \frac{\mu}{\rho} \nabla^2 \vec{v} + \vec{f} \quad \vec{z} = \frac{\partial \vec{v}}{\partial t} + \frac{\partial \vec{v}}{\partial x} \frac{dx}{dt} + \frac{\partial \vec{v}}{\partial y} v + \frac{\partial \vec{v}}{\partial z} w$$

$$\frac{\partial \vec{v}}{\partial t} + \frac{\partial \vec{v}}{\partial x} u + \frac{\partial \vec{v}}{\partial y} v + \frac{\partial \vec{v}}{\partial z} w = -\frac{1}{\rho} \text{grad}(\rho) + \frac{\mu}{\rho} \text{div}(\text{grad}(\vec{v})) + \vec{f}$$

non lineari

$$x \left\{ \begin{aligned} \frac{\partial u}{\partial t} + \frac{\partial u}{\partial x} u + \frac{\partial u}{\partial y} v + \frac{\partial u}{\partial z} w &= -\frac{1}{\rho} \frac{\partial \rho}{\partial x} + \frac{\mu}{\rho} \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right) + f_x \end{aligned} \right.$$

$$y \left\{ \begin{aligned} \frac{\partial v}{\partial t} + \frac{\partial v}{\partial x} u + \frac{\partial v}{\partial y} v + \frac{\partial v}{\partial z} w &= -\frac{1}{\rho} \frac{\partial \rho}{\partial y} + \frac{\mu}{\rho} \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right) + f_y \end{aligned} \right.$$

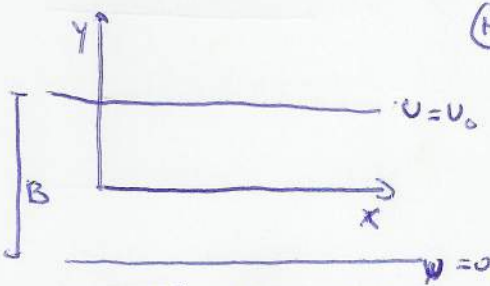
$$z \left\{ \begin{aligned} \frac{\partial w}{\partial t} + \frac{\partial w}{\partial x} u + \frac{\partial w}{\partial y} v + \frac{\partial w}{\partial z} w &= -\frac{1}{\rho} \frac{\partial \rho}{\partial z} + \frac{\mu}{\rho} \left(\frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right) + f_z \end{aligned} \right.$$

$$\text{div}(\vec{v}) = 0 \quad - \quad \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

MOTO LAMINARE:

1) **LASTRA SCORREVOLE**; ρ grad(p) dato e cost

(H) Newtoniano, incomprimibile, moto staz, $\vec{F}=0, v=0$



Scrivo Navier-Stokes lungo $l_z \times e_y + \text{cost}$

$$\vec{a} = -\frac{1}{\rho} \text{grad}(p) + \frac{\mu}{\rho} \nabla^2(\vec{v})$$

x: $\frac{\partial v}{\partial t} + \frac{\partial v}{\partial x} u + \frac{\partial v}{\partial y} v + \frac{\partial v}{\partial z} w = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \frac{\mu}{\rho} \nabla^2 v$

y: $\frac{\partial v}{\partial t} + \frac{\partial v}{\partial x} u + \frac{\partial v}{\partial y} v + \frac{\partial v}{\partial z} w = -\frac{1}{\rho} \frac{\partial p}{\partial y} + \frac{\mu}{\rho} \nabla^2 v$

cont: $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \Rightarrow \frac{\partial u}{\partial x} = 0$

$\frac{\partial u}{\partial x} = 0 \rightarrow l_z$ velocità non varia lungo x
 $\frac{1}{\rho} \frac{\partial p}{\partial y} = 0 \rightarrow l_x$ pressione non varia lungo y

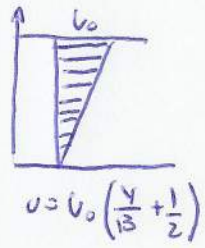
$\frac{\mu}{\rho} \frac{\partial^2 u}{\partial y^2} = \frac{1}{\rho} \frac{\partial p}{\partial x} \rightarrow$ tutto che p è f di x e u è f di y \Rightarrow derivabile l'altro

(HP) $p = \text{cost}$ e $p = -\infty \rightarrow \frac{\partial p}{\partial x} = \text{cost}$

$$\mu \frac{d^2 u}{dy^2} = \frac{dp}{dx} \xrightarrow{\text{integro}} \mu \frac{du}{dy} = \frac{C_1}{2} y \xrightarrow{\text{integro}} u = C_1 y + C_2$$

$$\begin{cases} u(\frac{B}{2}) = U_0 \rightarrow C_1 = \frac{2U_0}{B} \\ u(\frac{B}{2}) = 0 \rightarrow C_2 = -\frac{U_0}{2} \end{cases}$$

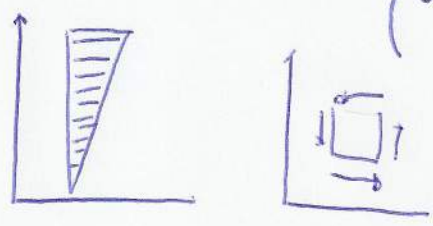
$$u = U_0 \left(\frac{y}{B} + \frac{1}{2} \right)$$



SPURTO

$$\underline{\underline{\Phi}} = p \underline{\underline{I}} - 2\mu \underline{\underline{D}} = \begin{bmatrix} p & -\mu \frac{u}{B} \\ -\mu \frac{u}{B} & p \end{bmatrix}$$

$$T = -2\mu \frac{1}{2} \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \rightarrow T = -\mu \frac{u}{B}$$



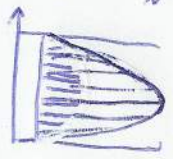
2) **LASTRA FERMA**, grad(p) dato

$$\mu \frac{d^2 u}{dy^2} = \frac{dp}{dx} \quad \text{tutto che } \frac{\partial p}{\partial x} = \text{cost} \Rightarrow \frac{\partial}{\partial x} \left(\frac{p}{\rho} \right) = +\gamma - \gamma$$

$$\mu \frac{d^2 u}{dy^2} = -\gamma \gamma \xrightarrow{\text{integro}} \mu \frac{du}{dy} = -\frac{\gamma \gamma}{2} y + C_1 \xrightarrow{\text{integro}} u = -\frac{\gamma \gamma}{2\mu} \frac{y^2}{2} + C_1 y + C_2$$

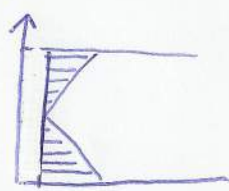
$$\begin{cases} u(\frac{B}{2}) = 0 \rightarrow C_1 = 0 \\ u(\frac{B}{2}) = 0 \rightarrow C_2 = \frac{\gamma \gamma B^2}{2\mu \cdot 4} \end{cases}$$

$$u = \frac{\gamma \gamma}{2\mu} \left(\frac{B^2}{4} - y^2 \right)$$



SPURTO

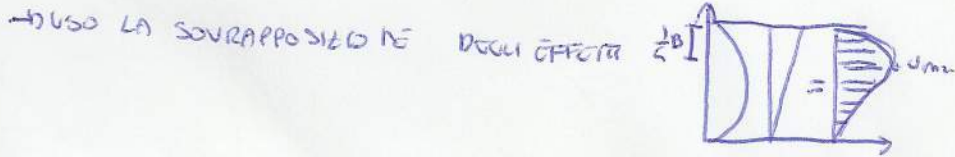
$$\underline{\underline{\Phi}} = p \underline{\underline{I}} - 2\mu \underline{\underline{D}} = \begin{bmatrix} p & \gamma \gamma y \\ \gamma \gamma y & p \end{bmatrix}$$



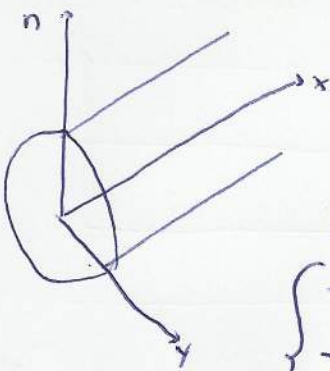
$$T = 0 - 2\mu \frac{1}{2} \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) = \gamma \gamma y$$

(NA) è costante di p non è f di y lo spurto

3) **MOTO LAN**: LAN movimento + GRAD DI PRESSIONE



TUTTO IN TUBAZIONI CIRCOLARI CILINDRICHE



HP: STAT $F = -\gamma \nabla z$ $v_m = v = 0$

$$\begin{cases} \bar{z} = \frac{1}{\rho} \text{grad}(p) + \frac{\mu}{\rho} \nabla^2(\vec{v}) + \vec{f} \\ \text{div}(\vec{v}) = 0 \end{cases}$$

CUN VARIE semplificazioni benali dovute alle ipotesi

$$\begin{cases} -\frac{1}{\rho} \frac{\partial p}{\partial x} + \frac{\mu}{\rho} \left(\frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right) - \gamma \frac{\partial z}{\partial x} = 0 \\ -\frac{1}{\rho} \frac{\partial p}{\partial y} - \gamma \frac{\partial z}{\partial y} = 0 \quad \frac{\partial}{\partial y} \left(\frac{p}{\rho} + z \right) = 0 \\ -\frac{1}{\rho} \frac{\partial p}{\partial z} - \gamma \frac{\partial z}{\partial z} = 0 \quad \frac{\partial}{\partial z} \left(\frac{p}{\rho} + z \right) = 0 \\ \frac{\partial u}{\partial x} = 0 \end{cases}$$

→ la distribuzione idraulica lungo le normali
→ lungo x non variaz velocità

$$\frac{\mu}{\rho} \left(\frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right) = \gamma \frac{\partial}{\partial x} \left(\frac{p}{\rho} + z \right)$$

→ $\frac{\partial u^2}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} = -\frac{\mu \gamma}{\rho} \frac{1}{R} \frac{\partial}{\partial R} \left(R \frac{\partial u}{\partial R} \right) + \frac{1}{R^2} \frac{\partial^2 u}{\partial \theta^2} = -\frac{\mu \gamma}{\rho}$

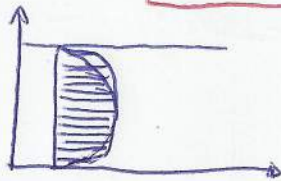
→ $\frac{\partial}{\partial R} \left(R \frac{\partial u}{\partial R} \right) = -\frac{\mu \gamma R}{2} \xrightarrow{\text{integro}} R \frac{du}{dR} = -\frac{\mu \gamma}{2} R^2 + C_1$

AL centro (R=0) $v = \text{max} \Rightarrow \frac{du}{dR} = 0 \quad R=0$
 \Downarrow
 $C_1 = 0$

integro → $u = -\frac{\mu \gamma}{4\nu} \frac{R^2}{2} + C_2$

→ In $R=R_0$ $u=0$ CUNO DI APPREZZO

$u = \frac{\mu \gamma}{4\nu} (R_0^2 - R^2)$



$C_2 = \frac{\mu \gamma}{4\nu} R_0^2$

$v_m = \frac{1}{A} \int u dA = \frac{v_{max}}{2} = \frac{\mu \gamma}{4\nu} \frac{R_0^2}{2} = \frac{\mu \gamma}{4\nu} \frac{D^2}{4}$

$v_m = \frac{\mu \gamma}{4\nu} \frac{D^2}{4} \rightarrow \gamma = \frac{32 \mu}{\rho D} \frac{v_m}{D}$ LEGEME LINEARE

→ $\gamma = \frac{32 \mu}{\rho \gamma D} \frac{v_m}{D} \frac{v_m \cdot v_m}{D^2}$

→ $\gamma = \frac{64}{Re} \frac{v_m^2}{2 \rho D}$ → il legame con v_m è invece lineare solo che esprimendolo in il termine cinetico cioè v_m^2 ma un v_m e un γ con Re

SFORZO

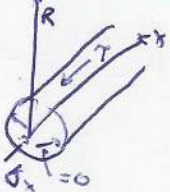
$\Phi = p \bar{z} - 2\mu D$

$T_{Rz} = 2\mu \frac{1}{2} \left(\frac{\partial u}{\partial R} + \frac{\partial R}{\partial x} \right)$

$T_{Rz} = \mu \frac{-\mu \gamma R}{2\mu} = -\mu \gamma \frac{R}{2}$

$\sigma_x = p \quad \sigma_R = p$

PANCA LATENTE



LUNGO IL PIANO yz

FACCE

$T_{xy} = -2\mu D_{xy} = -2\mu \frac{1}{2} \left(\frac{\partial u}{\partial y} + \frac{\partial y}{\partial x} \right) = -\mu \left(\frac{du}{dR} \frac{\partial R}{\partial y} \right)$

$\frac{du}{dR} = -\frac{\mu \gamma}{4\nu} 2R \quad R = \sqrt{x^2 + y^2} \quad \frac{\partial R}{\partial y} = \frac{y}{R} \quad \frac{\partial R}{\partial x} = \frac{x}{R}$

$-\mu \frac{du}{dR} \frac{\partial R}{\partial y} = -\mu \frac{-2\mu \gamma}{4\nu} 2R \frac{y}{R} = \frac{\mu \gamma y}{2}$

ANALOGO σ_{xy} (*)



$\tau = \sqrt{\sigma_{xy}^2 + \sigma_{yx}^2} = \frac{\mu \gamma R}{2}$ (*)

Si vede che le τ sono opposte, lo sforzo di sfurto NON è nullo ma solo l'azione ^{totale}

$T_x = \frac{1}{A_x} \int \tau dA_x = 0$

$T_y = \int \mu \frac{\partial u}{\partial x} dA$

$T_R = \int \sigma_{Rz} dA_R = \frac{\mu \gamma R_0}{2} 2R_0 DL = \mu \gamma R_0^2 DL$

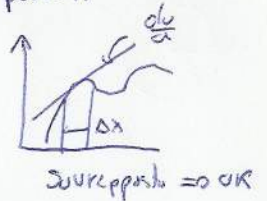
8 FOND SULLA PANCA LATENTE (21)

FLUIDI TURBOLENTI

OK

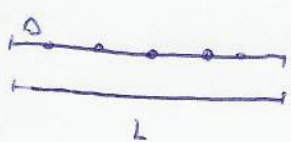
Le equazioni di Navier-Stokes non sono facilmente risolvibili nel continuo, dunque si rende il campo discreto, creando una griglia, e trovando le sol nei punti. Si moltiplicano variabili ed equazioni ma si trova una sol.

La scelta del passo della griglia e acc quando $\frac{du}{dx} = \lim_{\Delta x \rightarrow 0} \frac{\Delta u}{\Delta x}$



più Δx è piccolo + aumenta la precisione

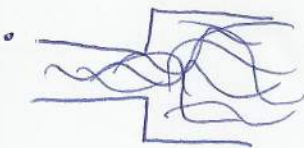
La griglia dipende dal grado della turbolenza, ma questo lo conosce dopo aver tenuto le sol
 mezzo vortici = L (scala) vortici interni = l (scala) microvortici = λ (scala)



$$\begin{cases} N \gg L \\ \Delta < \lambda \end{cases} \quad N > \frac{L}{\lambda} \quad N > Re^{\frac{3}{4}} \quad \text{in 3D} \quad Re^{\frac{9}{4}}$$

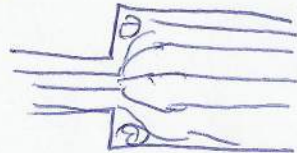
↑ numero minimo di passi

↑ numero minimo di vortici

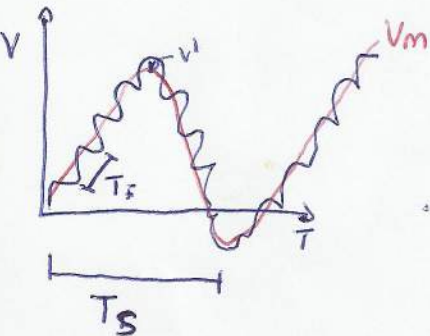


NON HO INTERESSE A CONOSCERE I VALORI ISTANTANEI, BASTA QUELLO NON

⇒



STUDIAMO LA velocità zero una periodicità T_s che contiene un'alta periodicità T_f



Dovremmo studiare il problema in un intervallo di tempo $T_f < T < T_s$

→ RISCIVO OGNI GRANDEZZA COME

termine medio
Fluttuazione

$$\bar{V} = \bar{V}_m + \bar{V}'$$

$$\bar{V}_m = \frac{1}{T_s} \int_0^{T_s} \bar{V} dt$$

$$V_m = \frac{1}{T_s} \int_0^{T_s} V_m + V' dt = \frac{1}{T_s} \int_0^{T_s} V_m dt + \frac{1}{T_s} \int_0^{T_s} V' dt \Rightarrow V_m = \frac{1}{T_s} V_m T_s + \frac{1}{T_s} \int_0^{T_s} V' dt \Rightarrow \boxed{\frac{1}{T_s} \int_0^{T_s} V' dt = 0}$$

FLUTTUAZIONE A MEDIA NULLA

NAVIER-STOKES

$$\rho \frac{D\mathbf{u}}{Dt} = \rho \left(\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \frac{\partial \mathbf{u}}{\partial x} + v \frac{\partial \mathbf{u}}{\partial y} + w \frac{\partial \mathbf{u}}{\partial z} \right) = \mu \nabla^2 \mathbf{u} - \frac{1}{\rho} \frac{\partial p}{\partial x} + \mathbf{f}_x$$

$$\textcircled{1} \left(\frac{\partial u}{\partial t} \right)_m = \frac{1}{T} \int_0^T \frac{\partial u}{\partial t} dt = \frac{\partial}{\partial t} \left[\frac{1}{T} \int_0^T u_m dt \right] = \frac{\partial u_m}{\partial t}$$

$$\textcircled{2} \left(\frac{\partial u}{\partial x} u \right)_m = \left((u_m + u') \frac{\partial (u_m + u')}{\partial x} \right)_m = \left(u_m \frac{\partial u_m}{\partial x} \right)_m + \left(u_m \frac{\partial u'}{\partial x} \right)_m + \left(u' \frac{\partial u_m}{\partial x} \right)_m + \left(u' \frac{\partial u'}{\partial x} \right)_m = u_m \frac{\partial u_m}{\partial x} + \frac{1}{T} \int_0^T u' \frac{\partial u'}{\partial x} dt$$

↑ il prodotto di 2 FLUTTE ≠ 0

$$\textcircled{3} (\nabla^2 u)_m = \frac{1}{T} \int_0^T \nabla^2 u dt = \nabla^2 \left[\frac{1}{T} \int_0^T u dt \right] = \nabla^2 u_m$$

$$\frac{\partial u_m}{\partial t} + u_m \frac{\partial u_m}{\partial x} + \frac{1}{T} \int u' \frac{\partial u'}{\partial x} dt + v_m \frac{\partial u_m}{\partial y} + \frac{1}{T} \int v' \frac{\partial u'}{\partial y} dt + w_m \frac{\partial u_m}{\partial z} + \frac{1}{T} \int w' \frac{\partial u'}{\partial z} dt = \frac{\mu}{\rho} \nabla^2 u_m + \frac{1}{\rho} \frac{\partial p_m}{\partial x} + f_{xm}$$

$$\frac{1}{T} \int \left(u' \frac{\partial u'}{\partial x} + v' \frac{\partial u'}{\partial y} + w' \frac{\partial u'}{\partial z} \right) dt \text{ non } d \quad \frac{\partial(u'u')}{2} = u' \frac{\partial u'}{\partial x} + v' \frac{\partial u'}{\partial x}$$

$$- \frac{1}{T} \int \left(u \frac{\partial(u'u')}{\partial x} - \frac{\partial u'u'}{\partial x} + v \frac{\partial(u'u')}{\partial y} - u \frac{\partial(v'u')}{\partial y} + \frac{\partial(w'u')}{\partial z} - \frac{\partial(w'u')}{\partial z} \right) dt$$

SPARISCONO con le eq di CONT $\begin{cases} \frac{\partial u_m}{\partial x} + \frac{\partial u_m}{\partial y} + \frac{\partial u_m}{\partial z} = 0 \\ \frac{\partial v_m}{\partial x} + \frac{\partial v_m}{\partial y} + \frac{\partial v_m}{\partial z} = 0 \end{cases} \Rightarrow \frac{\partial(u'u')}{\partial x} + \dots = 0$

$$\Rightarrow \frac{\partial u_m}{\partial t} + \frac{u_m}{\partial x} u_m + \frac{\partial v_m}{\partial y} v_m + \frac{\partial w_m}{\partial z} w_m + \frac{1}{T} \frac{\partial}{\partial x} \int_0^T u' u' + \frac{1}{T} \frac{\partial}{\partial y} \int_0^T v' v' + \frac{1}{T} \frac{\partial}{\partial z} \int_0^T w' w' = \frac{1}{\rho} \frac{\partial p_m}{\partial x} + \nabla^2 u_m + f_{xm}$$

EQUAZIONI DI REYNOLDS

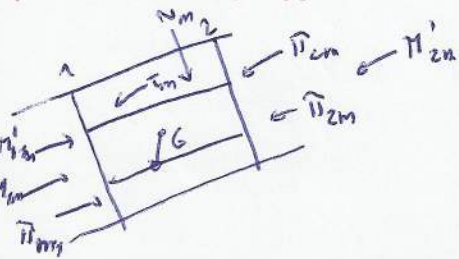
SFORZO

$$G + \Pi_p + \Pi_\mu + \Pi + J$$

$$G_n + \Pi_{pn} + \Pi_{\mu n} + \Pi + \Pi'_n + I_m = 0$$

Flusso di quantità di moto totale delle perturbazioni

PIU' REOLO STAZ.



$$M'_{1m} = \frac{1}{T} \int (u' v')_m dA$$

u, v in $A_1 \neq u, v$ in A_2
 $\frac{1}{2}$ la loro media è uguale
 $\Pi'_{1n} = \Pi'_{n1}$ così annullano

$$T = \gamma W J_m$$

$$T_{mx} = -\gamma W J_m = T_N + \Pi'_m x$$

$$T_{mx} = T_{\mu x} + M'_m x$$

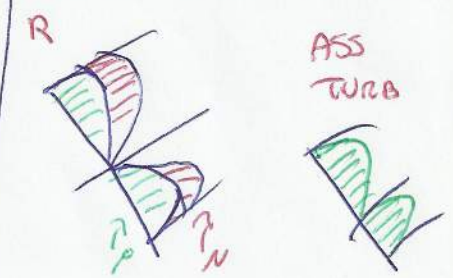
$$\hat{T}_{mx} = \frac{T_{mx}}{2\pi r L} = \frac{-\gamma \pi r^2 K J_m}{2\pi r L} = \frac{-\gamma r J_m}{2} = T_{\mu x} + \tau_p$$

$$\hat{T}_{\mu x} = \tau \mu_{brx} = \mu \frac{du_m}{dr} \quad \leftarrow \text{viscoso} \rightarrow \text{Newton}$$

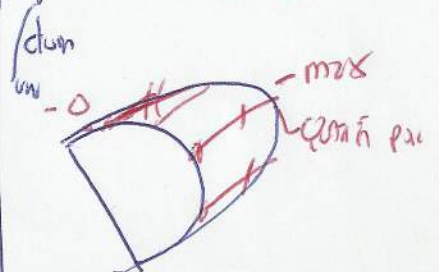
$$\hat{T}_p = \frac{M'_m}{SIP} = \rho \int_{A_2} (u' v')_m dA \quad \leftarrow \frac{\Pi'_m}{SIP}$$

$$\boxed{T = \mu \frac{du_m}{dr} + \rho \int_{A_2} (u' v')_m dA = \frac{\gamma R J_m}{2}} \quad (23)$$

SITO DI SFORZO AL VANTO DI

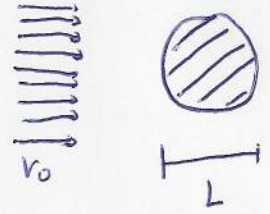


PROFILLO VELOCITA'



IL PROFILLO TURBOLTO È
 uguale a quello viscoso con
 meno una quantità max al centro

EQ DI EULERO E STOKES $\frac{\partial \vec{v}}{\partial t} + u \frac{\partial \vec{v}}{\partial x} + v \frac{\partial \vec{v}}{\partial y} + w \frac{\partial \vec{v}}{\partial z} = -\frac{1}{\rho} \text{grad } p + \frac{\mu}{\rho} \nabla^2 \vec{v} + \vec{f}$



Voglio studiare il moto nel caso di fluido newtoniano, incomprimibile e senza viscosità di L, v_0, ρ, μ
 $\Rightarrow 10^9$ simulazioni minime \rightarrow semplificare

1) moto stazionario $\frac{\partial \vec{v}}{\partial t} = 0$

2) Adimensionalizzare $\rightarrow (\rho, v_0, L)$

$\vec{v}^* = \frac{\vec{v}}{v_0} \rightarrow u^* = \frac{u}{v_0} \quad v^* = \frac{v}{v_0} \quad w^* = \frac{w}{v_0}$

$x^* = \frac{x}{L}$

$-\frac{1}{\rho} \text{grad}(p) + \vec{f} = -\frac{1}{\rho} \text{grad } p - g \text{grad } z = -\frac{1}{\rho} \nabla(p + \rho g z)$

$\tilde{p} = p + \rho g z \leq \frac{\rho v_0^2}{2}$ una pressione $-\frac{1}{\rho} \nabla(\tilde{p})$

$\tilde{p}^* = \frac{\tilde{p}}{\rho v_0^2}$

$\rightarrow \frac{\partial \vec{v}^*}{\partial t^*} + u^* \frac{\partial \vec{v}^*}{\partial x^*} + v^* \frac{\partial \vec{v}^*}{\partial y^*} + w^* \frac{\partial \vec{v}^*}{\partial z^*} = -\frac{1}{Re} \nabla^{*2} \vec{v}^* + \frac{1}{Re} \nabla^{*2} \vec{v}^*$

$[u^* \frac{\partial u^*}{\partial x^*} + v^* \frac{\partial v^*}{\partial y^*} + w^* \frac{\partial w^*}{\partial z^*}] = -\nabla^{*2} \tilde{p}^* + \frac{1}{Re} \nabla^{*2} \vec{v}^*$

$\nabla^{*2} \tilde{p}^* = \frac{1}{Re} \nabla^{*2} \vec{v}^* - \vec{a}_c^*$
 $Re \rightarrow 0 \rightarrow \text{cont } \nabla^{*2} \vec{v}^*$
 $Re \rightarrow \infty \rightarrow \text{cont } \vec{a}_c^*$

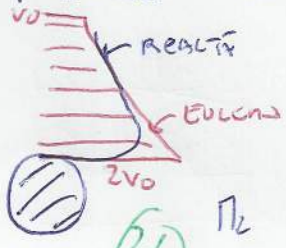
$\nabla \tilde{p}^* = \frac{1}{Re} \nabla^{*2} \vec{v}^* \Rightarrow \frac{L}{\rho v_0^2} \nabla \tilde{p} = \frac{1}{\rho \frac{v_0 L}{\mu}} \frac{1}{v_0} \nabla^2 \vec{v} \Rightarrow \nabla \tilde{p} = \mu \nabla^2 \vec{v}$
LEGGI DI STOKES
 Per $Re \rightarrow 0$

\rightarrow Trovo che $p = f(\mu, L, v_0)$ per $Re \rightarrow 0$

$\Pi_p = \frac{F}{\mu \frac{v_0 L^2}{\rho}} = \text{cost} \rightarrow$ se ho Re bassi sento ovunque l'effetto di μ solo all'infinito le velocità hanno w



$Re \rightarrow \infty$
 $\nabla \tilde{p}^* = -\vec{a}_c^* \rightarrow \frac{L}{\rho v_0^2} \nabla \tilde{p} = -\frac{L}{\rho v_0^2} \vec{a}_c \Rightarrow \nabla \tilde{p} = -\rho \vec{a}_c \Rightarrow \nabla(p + \rho g z) = -\rho \vec{a}_c$
 $\nabla p = -\rho (-g \vec{e}_z - \vec{a}_c)$



\Rightarrow L'eq di Eulero non prende in esame μ quindi per la continuità la velocità raddoppia quando $v \uparrow$ e ho $Re \uparrow$ la EULERO FUNGIONE vicino all'assetto per l'inerzia ho v bassi e $Re \downarrow \Rightarrow$ STATO LIMITE

$\nabla p = -\rho (\vec{F} - \vec{a}_c)$

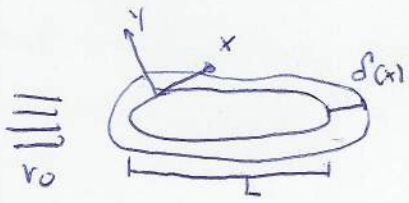
EQ DI EULERO
 Per $Re \rightarrow \infty$

ZONA DI STRATO LIMITE → Lo strato dove la velocità è compresa tra 0 e il 99%

E ciò che unisce l'equazione di Navier-Stokes (μ) all'equazione di Eulero.

L'equazione di Eulero funziona all'esterno, di moto non viscoso o non turbolento. **(STRATO LIMITE COMPLETAMENTE SVILUPPATO)**

STRATO COMPLETAMENTE SVILUPPATO ⇒ $Re \rightarrow +\infty$



$$U^* = \frac{U}{v_0} \quad V^* = \frac{V}{v_0}$$

Eq CONT: $\frac{\partial U}{\partial x} + \frac{\partial V}{\partial y} = 0$

$$\frac{v_y}{L} \frac{\partial U^*}{\partial x^*} + \frac{v_x}{L} \frac{\partial V^*}{\partial y^*} = 0$$

$$\begin{cases} \nabla^* \tilde{p}^* = \frac{\nabla^{*2} \tilde{v}^*}{Re} - \left(U^* \frac{\partial U^*}{\partial x^*} + V^* \frac{\partial V^*}{\partial y^*} \right) \\ \frac{\partial U^*}{\partial x^*} + \frac{\partial V^*}{\partial y^*} = 0 \end{cases}$$

lungo x $\frac{\partial \tilde{p}^*}{\partial x^*} = \frac{1}{Re} \left(\frac{\partial^2 U^*}{\partial x^{*2}} + \frac{\partial^2 U^*}{\partial y^{*2}} \right) - \left(U^* \frac{\partial U^*}{\partial x^*} + V^* \frac{\partial U^*}{\partial y^*} \right)$

$x^* = \frac{x}{L} = \mathcal{O}(1)$ $y^* = \frac{y}{L} = \mathcal{O}(\epsilon)$ $v^* = \frac{v}{v_0} = \mathcal{O}(1)$ $\epsilon = \frac{d}{L} \ll 1$ ← esatto Re

CONT $\frac{\partial U^*}{\partial x^*} + \frac{\partial V^*}{\partial y^*} \Rightarrow \frac{\mathcal{O}(1)}{\mathcal{O}(1)} + \frac{\mathcal{O}(\epsilon)}{\mathcal{O}(\epsilon)} \quad V^* = \mathcal{O}(\epsilon)$

NAVIER STOKES

$$\frac{\partial^2 U^*}{\partial x^{*2}} + \frac{\partial^2 U^*}{\partial y^{*2}}$$

⇒ $\frac{\mathcal{O}(1)}{\mathcal{O}(1)} + \frac{\mathcal{O}(1)}{\mathcal{O}(\epsilon^2)}$ ← TRASCURRIBILE

⇒ Ha massima diffusione lungo la y

$$U^* \frac{\partial U^*}{\partial x^*} + V^* \frac{\partial U^*}{\partial y^*} \Rightarrow \mathcal{O}(1) + \mathcal{O}(\epsilon) \frac{\mathcal{O}(1)}{\mathcal{O}(\epsilon)}$$

⇒ Poiché sono sommate e chiaro avere le stesse dimensioni

⇒ $\frac{1}{Re} = \mathcal{O}(\epsilon^2) \Rightarrow Re \rightarrow +\infty$

$$\frac{1}{Re} \mathcal{O}(\epsilon^2) \rightarrow \frac{1}{Re} \mathcal{O}\left(\frac{d}{L}\right)^2 \rightarrow \frac{1}{\sqrt{Re}} \mathcal{O}\left(\frac{d}{L}\right)$$

⇒ LUNGO x $\begin{cases} \frac{\partial \tilde{p}^*}{\partial x^*} = \frac{1}{Re} \frac{\partial^2 U^*}{\partial y^{*2}} - \left(U^* \frac{\partial U^*}{\partial x^*} + V^* \frac{\partial U^*}{\partial y^*} \right) \quad \rightarrow \frac{\partial \tilde{p}^*}{\partial x^*} = \mathcal{O}(1) \\ \frac{\partial U^*}{\partial x^*} + \frac{\partial V^*}{\partial y^*} = 0 \end{cases}$

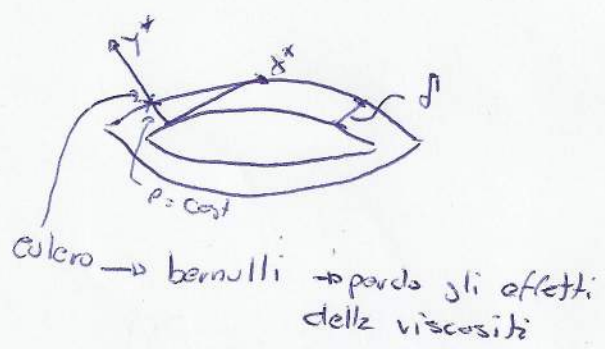
⇒ LUNGO y $\frac{\partial \tilde{p}^*}{\partial y^*} = \frac{1}{Re} \left(\frac{\partial^2 U^*}{\partial x^{*2}} + \frac{\partial^2 V^*}{\partial y^{*2}} \right) - \left(U^* \frac{\partial V^*}{\partial x^*} + V^* \frac{\partial V^*}{\partial y^*} \right)$

$\mathcal{O}(\epsilon^2) \left(\mathcal{O}(\epsilon) + \frac{\mathcal{O}(\epsilon)}{\mathcal{O}(\epsilon^2)} - \left(\mathcal{O}(1) \mathcal{O}(\epsilon) + \mathcal{O}(\epsilon) \frac{\mathcal{O}(\epsilon)}{\mathcal{O}(\epsilon)} \right) \right) = \mathcal{O}(\epsilon)$

LUNGO y il gradiente di pressione è trascurabile!! (25)

EQ INDEFINITA DI STRATO LIMITE

$$\begin{cases} \frac{\partial \tilde{p}^*}{\partial x^*} = \frac{1}{Re} \frac{\partial^2 U^*}{\partial y^{*2}} - \left(u^* \frac{\partial^2 U^*}{\partial x^{*2}} + v^* \frac{\partial^2 U^*}{\partial y^{*2}} \right) \\ \frac{\partial \tilde{p}^*}{\partial y^*} = 0 \quad (\text{NUOVO STATO LIMITE } p = \text{cost}) \\ \frac{\partial u^*}{\partial x^*} + \frac{\partial v^*}{\partial y^*} = 0 \end{cases}$$



$$z + \frac{p}{\rho} + \frac{V^2}{2} = \text{cost} \rightarrow z + \frac{p}{\rho} + \frac{V^2}{2} = c_1 \rightarrow \tilde{p} + \frac{V^2}{2} \rho = c_1 \Rightarrow \frac{\partial}{\partial x^*} \left(\tilde{p} + \frac{V^2}{2} \rho \right) = 0$$

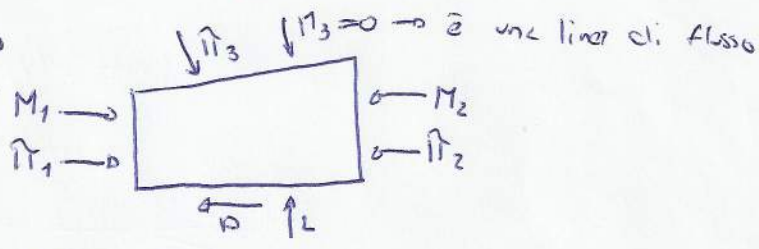
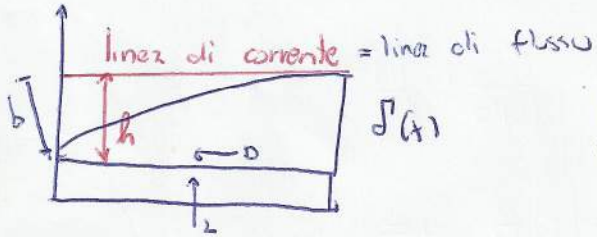
\rightarrow Adimensionalizzato questo interno $\frac{\partial}{\partial x^*} \left(\frac{\tilde{p}}{\rho V_0} + \frac{V^2}{2} \right) = 0 \rightarrow \frac{\partial}{\partial x^*} \left(\tilde{p}^* + \frac{V^{*2}}{2} \right) = 0$

$$\frac{\partial}{\partial x^*} \tilde{p}^* = -\frac{1}{2} \frac{\partial}{\partial x^*} (V^{*2}) = V^* \frac{\partial V^*}{\partial x^*} = \frac{\partial}{\partial x^*} (\tilde{p}^{*1})$$



\rightarrow Eq governate solo delle curve di monte ma non di quelle di valle!

CALCOLO DEL DRAG CON EQUILIBRIO LOCALE



$$\text{lungo } x: |\bar{M}_1| + |\bar{\pi}_1| + \bar{\pi}_3^* = |\bar{M}_2| + |\bar{\pi}_2| + |\bar{D}|$$

nelle zone di stretto limite $p = \text{cost}$

$$\bar{\pi}_1 = p_0 h b = p_0 A_1$$

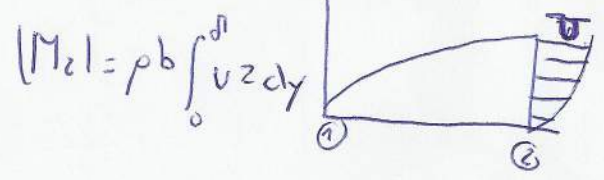
$$\bar{\pi}_2 = p_0 \int(x) b = p_0 A_2$$

$$\bar{\pi}_3 = p_0 A_3 = p_0 (A_2 - A_1)$$

$$\bar{\pi}_{3x} = p_0 A_3^* = p_0 (A_2 - A_1)$$

$$\bar{\pi}_1 + \bar{\pi}_2 + \bar{\pi}_3 = p_0 (A_1 - A_2 + A_2 - A_1) = 0$$

$$\bar{M} = \rho \int_a^b \vec{V} V_m dA \quad |M_1| = \rho U U h b$$



Perche $Q_1 = Q_2 \rightarrow b h U = b \int_0^d u dy$

$$|M_1| = \rho b U \int_0^d u dy$$

$$|\bar{D}| = |M_1| - |M_2| = \rho b U^2 \int_0^d \frac{u}{U} \left(1 - \frac{u}{U} \right) dy$$

$$|M_2| = \rho b \int_0^d u^2 dy$$

$$\bar{D} = \rho b U^2 \theta$$

$$\frac{d\bar{D}}{dx} = b \tau \quad \rightarrow \quad b \tau = b \rho U^2 \frac{\theta}{dx}$$

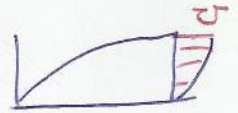
$$\tau = \rho U^2 \frac{\theta}{dx}$$

ADIMENSIONALIZZAZIONE

$$\frac{U}{U} = f\left(\frac{y}{\delta}\right)$$

2 CONDIZIONI AL CONTINNO

$$\begin{cases} f\left(\frac{y}{\delta}=0\right) = 0 \\ f\left(\frac{y}{\delta}=\delta\right) = 1 \end{cases} \rightarrow \text{in } \delta \text{ ho } u = U$$

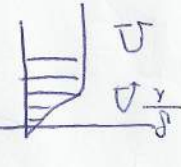


$$\theta = \int_0^\delta \frac{U}{U} \left(1 - \frac{U}{U}\right) dy \rightarrow \int_0^\delta f\left(\frac{y}{\delta}\right) \left[1 - f\left(\frac{y}{\delta}\right)\right] dy$$

CAMBIO DI VAR $\bar{Y} = \frac{y}{\delta} \quad d\bar{Y} = \frac{1}{\delta} dy$

$$\theta = \delta \int_0^1 f(\bar{Y}) [1 - f(\bar{Y})] d\bar{Y} = \delta C_1$$

CASO LINEARE: $C_1 = \int_0^1 Y(1-Y) dY = \int_0^1 (Y^2 - Y^3) dY = \left[\frac{Y^3}{3} - \frac{Y^4}{4}\right]_0^1 = \frac{1}{3} - \frac{1}{4} = \frac{1}{12}$



$$\tau = \rho U^2 \frac{\theta}{dx} = \rho U C_1 \frac{\delta}{dx}$$

DALLA LEGGE DI NEWTON

$$\begin{aligned} \tau &= \mu \frac{\partial u}{\partial y} \stackrel{\text{ADIMENSIONALIZZAZIONE}}{=} \mu U \frac{\partial}{\partial y} \left(\frac{u}{U}\right) \frac{d\bar{Y}}{dY} \\ &= \mu U \frac{\partial}{\partial \bar{Y}} \left[f(\bar{Y})\right] \frac{1}{\delta} = \mu U C_2 \frac{1}{\delta} \end{aligned}$$

$$\Rightarrow \rho U C_1 \frac{\delta}{dx} = \mu \frac{C_2}{\delta} \rightarrow \int_0^{\delta} \delta \cdot d\delta = \mu \frac{C_2/C_1}{\rho U} \int_0^{\delta} dx \rightarrow \frac{\delta^2}{2} = \mu \frac{C_2}{C_1 \rho U} x$$

$$\delta = \sqrt{2\mu \frac{C_2}{C_1 \rho U} x} \rightarrow \text{ADIMENSIONALIZZAZIONE} \quad \frac{\delta}{x} = \sqrt{\frac{2\mu \frac{C_2/C_1}{\rho U} x}{\rho U x^2}} = \sqrt{\frac{2 C_2/C_1}{Re}}$$

↳ Lo spessore di strato limite per qualsiasi θ in fun. di Re

$$|\bar{D}| = \rho b U^2 x \frac{\sqrt{2 C_2/C_1}}{\sqrt{Re}}$$

$$C_0 = \frac{|\bar{D}|}{\frac{1}{2} \rho U b x} = \frac{\rho b U^2 x \frac{\sqrt{2 C_2/C_1}}{\sqrt{Re}}}{\frac{1}{2} \rho U^2 b x} = \frac{\sqrt{2 C_2/C_1}}{\sqrt{Re}} = 2 \frac{\sqrt{2 C_2/C_1}}{\sqrt{Re}} \rightarrow \text{All'aumentare di } Re \text{ } C_0 \downarrow$$